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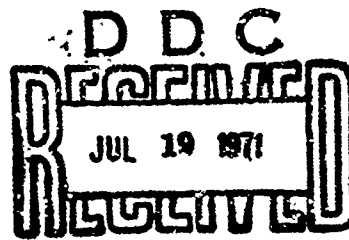
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**THEORETICAL GUN PROPELLANT  
THERMOCHEMICAL EVALUATION**

**GUNS AND ROCKETS BRANCH  
ADVANCED DEVELOPMENT DIVISION**

**TECHNICAL REPORT AFATL-TR-71-11**

**JANUARY 1971**



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# **Theoretical Gun Propellant Thermochemical Evaluation**

**Otto K. Heiney**

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## FOREWORD

This report has been generated under the advanced gun propellant evaluation analysis portion of Project 62602F 2560 and is presented as a state of the art advancement that can be applied to gun propellant research efforts. The study was conducted during the period February 1970 to January 1971.

This technical report has been reviewed and is approved.



CHARLES PETRIDES

Chief, Advanced Development Division

## ABSTRACT

A computer program is presented for computing the chemical equilibrium reaction products associated with gun propellant combustion. This program will provide a good first approximation of flame temperature, specific heat ratio, impetus, and mean molecular weight of the combustion products. The program as developed at the Air Force Armament Laboratory was based on a code used by the National Aeronautics and Space Administration Lewis Research Center. The minor changes to the program are discussed, some results from advanced solid propellant formulations calculations are presented, and a form of users manual for thermochemical programs and for the program to generate specific heat polynomials from JANAF tabular data is presented.

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# LIST OF ABBREVIATIONS AND SYMBOLS

$C_p$	Specific heat at constant pressure
$C_v$	Specific heat at constant volume
$E$	Internal energy
$F_p$	Propellant impetus
$G$	Gibbs free energy
$H$	Enthalpy
$K$	Gas conductivity
$M$	Molecular weight
$P$	Pressure
$R$	Gas constant
$S$	Entropy
$T$	Temperature
$T_{FP}$	Flame temperature at constant pressure
$T_{FV}$	Flame temperature at constant volume
$V$	Volume
$X_i$	Mole fraction
$\gamma$	Specific heat ratio
$\sigma$	Leonard-Jones force constant
$\Omega$	Leonard-Jones force constant
$\mu$	Gas viscosity

## SECTION I

### INTRODUCTION

The field of gun propellant development, which had been relatively static for many years, has recently begun to attract increased attention. The availability of an accurate theoretical thermochemical propellant performance computer program is of central importance to informed research and development efforts in this field. As a formulation screening tool, a few dollars of machine time can save hundreds of dollars of laboratory small-batch-mix effort by eliminating unpromising candidate formulations and providing a good first approximation to the primary important propellant parameters. These would include flame temperature, specific heat ratio, impetus, and mean molecular weight of the combustion products. To most expediently obtain a computer program for computing the chemical equilibrium reaction products, the Air Force Armament Laboratory modified an existing free-energy minimization rocket propellant performance program. The program selected was the one used by the National Aeronautics and Space Administration Lewis Research Center. This code<sup>(1)</sup> has a background of almost ten years of successful application. In addition, it was readily available and the JANAF specific heat data could be easily applied to the thermodynamic data tape. The program, as modified for gun propellant applications, was checked against established experimental data and other analytic chemical equilibrium computing techniques, with excellent agreement. Additionally, an algorithm was added which computes combustion gas viscosity and thermal conductivity by a Leonard-Jones potential technique.

The following sections of this report discuss the minor changes made to the Lewis approach, give some results from advanced solid propellant formulation calculations, and provide a form of users manual for the thermochemical programs and for the program to generate specific heat polynomials from JANAF tabular data<sup>(2)</sup>. Appendix I presents the Lewis program listing and Appendix II presents the polynomial fit program used at the Armament Laboratory.

## SECTION II

### FREE ENTHALPY EQUATIONS

This report will not discuss the mathematical techniques of chemical equilibrium computations. This task has effectively been accomplished in a recently issued monograph<sup>(3)</sup> which discusses in detail not only the Lewis technique but also several other commonly used approaches. This report will demonstrate only that, at chemical equilibrium, the Gibbs free energy,  $G$ , (or free enthalpy) will be a minimum.

From the First Law of Thermodynamics, in an irreversible process:

$$dE + pdv - Tds < 0 \quad (1)$$

or at equilibrium

$$dE + pdv - Tds = 0 \quad (2)$$

For a constant pressure and temperature, equation (2) becomes

$$d(E + pv - Ts) = 0 \quad (3)$$

$$G_T = H_T - T_1 S_1 \quad (4)$$

Equation (4) establishes the relation that the Gibbs free energy will be a minimum at equilibrium, and when coupled with the atomic species mass conservation equations, it provides a sufficient set for solution of the combustion species concentration and flame temperature (if the combustion pressure is specified). Then, to set up a minimization algorithm only requires a value for the heat of formation of the reactant compounds and tabular or polynomial data for the specified heat,  $C_p$ , enthalpy,  $H_T$ , and entropy,  $S_T$ , of the possible combustion products. These thermodynamic data can be obtained from reference 2 for most combustion products of interest: as

$$H_T - H_{298} = \int_{298}^T C_p dT \quad (5)$$

$$\text{and } S_T - S_{298} = \int_{298}^T \frac{C_p}{T} dT \quad (6)$$

Selecting a polynomial form for  $C_p$ , the terms  $H_T$  and  $S_T$  can be conveniently fitted to similar polynomials by performing the indicated integrations

$$\frac{C_p}{R} = a_1 + a_2 T + a_3 T^2 + a_4 T^3 + a_5 T^4 \quad (7)$$

$$\frac{H_T}{RT} = a_1 + 1/2 a_2 T + 1/3 a_3 T^2 + 1/4 a_4 T^3 + 1/5 a_5 T^4 + a_6/T \quad (8)$$

$$\frac{S_T}{R} = a_1 \ln T + a_2 T + 1/2 a_3 T^2 + 1/3 a_4 T^3 + 1/4 a_5 T^4 + a_7 \quad (9)$$

For a more precise fit, the Lewis program utilizes two sets of coefficients for each species, one in the temperature range  $0^\circ$  to  $1000^\circ K$  and the other from  $1000^\circ$  to  $6000^\circ K$ . Limits of species existence can be placed on the propellant data to restrict the range of polynomial applicability.

The primary change made to the Lewis algorithm was to additionally develop an approximate isochoric temperature from the isobaric temperature provided by the program. This requires the assumption that approximately the same species would form either in an isochoric or isobaric process, providing a similar total heat release. If these assumptions are warranted, then:

$$Q_R = C_p T_{FP} \quad (10)$$

$$Q_R = C_v T_{FV} \quad (11)$$

$$T_{FV} = C_p / C_v T_{FP} = \gamma T_{FP} \quad (12)$$

Once the isochoric flame temperature and mean molecular weight of the combustion products are known, the impetus is simply

$$F_p = \frac{R}{M} T_{FV} \quad (13)$$

where  $R = 2780 \text{ ft-lbs/lb-mole-}^\circ K$

The program also computes the constitutive products mole fractions as a function of the pressure ratio (or, for a gun system, of the velocity) if quasi-isentropic conditions are assumed.

Equation (13) indicates the importance of developing advanced propellants with lower molecular weight combustion products, if the impetus

of a propellant is to be increased without a corresponding flame temperature increase. High propellant flame temperatures are, of course, the prime limiting factor in developing an acceptable barrel life for automatic aircraft cannon having a high performance and a high rate of fire. Current single-base solid gun propellants display molecular weights in the order of 25. Table I illustrates the distinctive flame temperature advantage of lower molecular weights in obtaining cooler combustion conditions without sacrificing energy output.

TABLE I. FLAME TEMPERATURES AS A FUNCTION OF MOLECULAR WEIGHT AND IMPETUS				
Molecular Weight, Atomic Mass Units	Flame Temperature, °K, at Impetus, Ft-lb/lb			
	325,000	350,000	375,000	400,000
25	2980	2150	3380	3500
22	2570	2770	2970	3170
20	2340	2620	2700	2880
19	2220	2390	2570	2740
18	2110	2270	2430	2590
17	1990	2140	2290	2450

The very favorable performance data indicated by the lower right-hand entries in Table I are responsible for the continued advanced solid gun propellant development efforts. The test cases described in the following sections have resulted from calculations of two of the formulations now under contract investigation and from a comparison of results of two theoretical computations with experimental measurements of inservice propellants. All computations are performed at a standard reference pressure of 5,000 psia.

The first requirement for free energy computations is a reliable list of heats of formations for the constituents to be considered. Table II provides this data for the ingredients in the formulations discussed in this report. Additional tables are available in references 4 and 5.

TABLE II. HEATS OF FORMATION		
CONSTITUENT	EMPIRICAL FORMULA	HEATS OF FORMATION KILOCALORIES PER MOLE
Ammonium Nitrate	H <sub>4</sub> O <sub>3</sub> N <sub>2</sub>	-88.1
CTPB	C <sub>7</sub> H <sub>11</sub> O <sub>0.2</sub> N <sub>0.02</sub>	-5.0
Dibutylphthalate	C <sub>18</sub> H <sub>14</sub> O <sub>4</sub>	-200.0
Diphenylamine	C <sub>12</sub> H <sub>11</sub> N <sub>1</sub>	+27.6
DMDTH	C <sub>6</sub> H <sub>14</sub> O <sub>6</sub> N <sub>4</sub>	-94.0
Ethyl Acrylate	C <sub>5</sub> H <sub>8</sub> O <sub>2</sub>	-87.3
Ethyl Alcohol	C <sub>2</sub> H <sub>6</sub> O <sub>1</sub>	-66.3
Ethyl Centralite	C <sub>17</sub> H <sub>20</sub> O <sub>1</sub> N <sub>2</sub>	-34.2
Ethylene Dihydrazine	C <sub>2</sub> H <sub>10</sub> N <sub>4</sub>	+31.2
Glycol Dinitrate	C <sub>2</sub> H <sub>4</sub> O <sub>6</sub> N <sub>2</sub>	-58.7
Guanidine Nitrate	C <sub>1</sub> H <sub>6</sub> O <sub>3</sub> N <sub>4</sub>	-79.3
HMX	C <sub>4</sub> H <sub>8</sub> O <sub>8</sub> N <sub>8</sub>	+17.9
Nitrocellulose (12.6 percent N)	C <sub>24</sub> H <sub>30.2</sub> O <sub>39.4</sub> N <sub>9.8</sub>	-655.5
Nitrocellulose (12.7 percent N)	C <sub>24</sub> H <sub>30</sub> O <sub>40</sub> N <sub>10.0</sub>	-659.3
Nitrocellulose (13.15 percent N)	C <sub>24</sub> H <sub>29.5</sub> O <sub>41.3</sub> N <sub>10.6</sub>	-643.1
Nitrocellulose (13.75 percent N)	C <sub>24</sub> H <sub>29.3</sub> O <sub>41.4</sub> N <sub>10.7</sub>	-639.9
Nitroglycerine	C <sub>3</sub> H <sub>5</sub> O <sub>9</sub> N <sub>3</sub>	-85.3
Nitroguanidine	C <sub>1</sub> H <sub>4</sub> O <sub>2</sub> N <sub>4</sub>	-12.6
Polymethyl Vinyl Tetrazole	C <sub>4</sub> H <sub>6</sub> N <sub>4</sub>	+52.4
RDX	C <sub>3</sub> H <sub>6</sub> O <sub>6</sub> N <sub>6</sub>	+14.9
Potassium Sulfate	K <sub>2</sub> S <sub>1</sub> C <sub>4</sub>	-338.5
Triacetin	C <sub>9</sub> H <sub>14</sub> O <sub>6</sub>	-307.0
Triazoethanol	C <sub>2</sub> H <sub>5</sub> O <sub>1</sub> N <sub>3</sub>	+22.5
Triaminoguanidine Nitrate	C <sub>1</sub> H <sub>9</sub> O <sub>5</sub> N <sub>7</sub>	-11.5
Water	H <sub>2</sub> O <sub>1</sub>	-68.4

### SECTION III

#### COMPUTATION OF VISCOSITY AND CONDUCTIVITY

For gun propellant applications, it is often quite important to determine a theoretical value for the combustion gas conductivity and viscosity. These are particularly necessary if the convective gun barrel heating characteristics of the propellants are to be evaluated. To accomplish this task, the Leonard-Jones potential technique<sup>(6)</sup> was applied.

The viscosity for a single constitutive species is given by:

$$\mu_1 = 2.6693 \times 10^{-5} \sqrt{MT} / \sigma^2 \Omega \quad (14)$$

where T is the temperature, M is the molecular weight, and  $\sigma$  and  $\Omega$  are the Leonard-Jones force constants. The viscosity of the mixture is defined by

$$\mu_{MIX} = \sum_{i=1}^n \left( x_i \mu_i \right) \left( \sum_{j=1}^n x_j \phi_{ij} \right) \quad (15)$$

with n being the number of species considered and  $x_i$  being the mole fraction of the species. The value,  $\phi_{ij}$  is defined as

$$\phi_{ij} = \frac{1}{\sqrt{8}} \left( 1 + \frac{M_i}{M_j} \right)^{-1/2} \left[ 1 + \left( \frac{\mu_i}{\mu_j} \right)^{1/2} \left( \frac{M_j}{M_i} \right)^{1/4} \right]^2 \quad (16)$$

The thermal conductivity of a species is given as:

$$K_i = 1.9891 \times 10^{-4} \frac{\sqrt{T/M}}{\sigma^2 \Omega} \quad (17)$$

The mixture value is given as

$$K_{MIX} = \sum_{i=1}^n \left( x_i K_i \right) \left( \sum_{j=1}^n x_j \phi_{ij} \right) \quad (18)$$

This approach is strictly valid for only dilute mixtures of non-polar molecules. Five species are considered, (one of which,  $H_2O$ , is polar), and all have a dense gas system. Thus, the results contain only order of magnitude validity, but are none the less of value, considering the state of the art in mathematical modeling of the transient heat convection process in gun bores. Table III gives the species considered which are typically 98 to 99 percent of the combustion gas constituents.



TABLE III. LEONARD-JONES POTENTIAL PARAMETERS (FORCE CONSTANTS)			
Species	Molecular Weight, Atomic Mass Units	Viscosity, Grams/cm-sec	Conductivity, Cal/cm-sec-K
H <sub>2</sub>	2.016	2.915	38.0
N <sub>2</sub>	28.02	3.749	79.8
CO	28.01	3.706	88.
CO <sub>2</sub>	44.01	3.897	213.
H <sub>2</sub> O	18.0	2.824	230.9

Table IV consists of the  $\Omega - \frac{KT}{\epsilon}$  relations needed for the solution of Equations (14) and (17). The first column contains values for the relatively non-polar species such as H<sub>2</sub>, N<sub>2</sub>, CO, and CO<sub>2</sub>, while the second column has a corrected value for the highly polar H<sub>2</sub>O.

TABLE IV. REDUCED CROSS SECTION

KT/ε	NON-POLAR	POLAR		KT/ε	NON-POLAR	POLAR
1.0	1.5938	2.6199		7	0.8725	0.8946
1.2	1.4568	2.4257		8	0.8536	0.8422
1.4	1.3557	2.2713		9	0.8378	0.8043
1.6	1.2800	2.1413		10	0.8242	0.7760
1.8	1.2216	2.0263		11	0.8123	0.7544
2.0	1.1751	1.9217		12	0.8017	0.7376
2.2	1.1377	1.8258		13	0.7922	0.7243
2.4	1.1066	1.7373		14	0.7836	0.7134
2.6	1.0803	1.6559		15	0.7756	0.7045
2.8	1.0579	1.5812		16	0.7883	0.6971
3.0	1.0385	1.5126		32	0.6939	0.6462
3.2	1.0214	1.4499		64	0.6262	0.6033
3.4	1.0063	1.3926		128	0.5634	0.5528
3.6	0.9928	1.3401		256	0.5056	0.5006
3.8	0.9807	1.2922		512	0.4528	0.4505
4.0	0.9696	1.2485				
5.0	0.9265	1.0797				
6.0	0.8960	0.9694				

## SECTION IV

### INPUT FOR GUN PROPELLANT PROGRAM

The input data for the gun propellant program (Appendix I) can be divided into four general groups having code names as follows:

- 1) Thermodynamic data for the reaction products (THERMØ data).
- 2) Data pertaining to the reactants or propellants (REACTANTS data).
- 3) Special options related to chemical species present in the combusted gas (ØMIT/INSERT data).
- 4) Namelist data including the type of problem, pressure ratio and area ratio schedules, various options, etc. (NAMELISTS data).

The required order of the data cards is:

- 1) One card with the code word THERMØ punched in columns 1 to 6.
- 2) THERMØ data.
- 3) REACTANTS card. Number of reactants right adjusted in columns 1 to 3 and number of cases right adjusted in columns 4 to 6.
- 4) ØMIT and/or INSERT data.
- 5) One card containing up to 80 columns of alphanumeric identification data.
- 6) NAMELISTS data.

For any particular problem there may be multiple REACTANTS cards. Each set of REACTANTS cards may be followed by multiple NAMELISTS input cards. Each type of input data is discussed in detail in the following sections.

#### 1. THERMØ DATA

The thermodynamic data for the reaction products may be read either from cards or from magnetic tape. When tape input is used, both the THERMØ code card and all THERMØ data cards must be omitted. It is anticipated that most users will prefer the magnetic tape since this reduces the number of cards which must be handled. The card format for the THERMØ data is described in Section V. Use of the tape input requires no action on the part of the user, once the required data is established on the tape.

#### 2. REACTANTS DATA

REACTANTS data is required for all problems. Following the code card there should follow one card for each reactant species being considered, with a maximum of 15 allowed. Each reactant card, after the code card, contains the following information:

- a. The chemical formula for the species.
- b. Either the number of moles of the reactant or the relative weight. The relative weight is the weight of each fuel or oxidizer expressed as a fraction of the total fuel or oxidizer.
- c. The enthalpy of the species expressed in calories per mole. (This is not required for an assigned temperature problem. See Section IV.4 for description of assigned temperature problem.)
- d. The state of the reactant (gas, liquid, or solid).
- e. The temperature associated with the enthalpy.
- f. Designation of each reactant species as either a fuel or an oxidizer. (The program then combines all fuels into an effective fuel and all oxidizers into an effective oxidizer.)
- g. The reactant species density. (This information is optional and may be omitted. If densities are input for all reactants, the program calculates a density for the overall system.)
- h. Multiple cases with identical reactants are identified by the reactants code card and the preceding data need not be repeated.

The reactant information is arranged on a card. Standard chemical alphabetic symbols are required for the chemical elements (i.e., H for hydrogen, HE for helium, LI for lithium, BE for beryllium, etc.). Each reactant may be composed of no more than five distinct chemical elements. Each chemical element is allowed two columns (columns 1 and 2, 10 and 11, 19 and 20, 28 and 29, and 37 and 38) for its symbol. For those elements whose symbol consists of a single letter, the symbol must be placed in the left-most (left adjusted) of the two columns. The formula number (the number of atoms of each element in a reactant) is to appear in the columns immediately following the chemical symbol (i.e., columns 3 to 9, 12 to 18, 21 to 27, 30 to 36, and 39 to 45). The formula number may appear anywhere within the seven column field, and a decimal point must be used for each number. Note that the exponent numeric form, or E format, may not be used here. Also note that for a given reactant an individual element may appear only once (empirical formula). Thus, a compound such as furfuryl alcohol, whose formula might be written as  $C_4H_3O \cdot CH_2OH$  to represent its structure, must be treated as though it were  $C_5H_6O_2$  or  $O_2H_6C_5$ , etc. The order of the elements is immaterial for this program.

The relative weight of each reactant should be placed in columns 46 to 52. The number may appear anywhere in these columns, a decimal point must be used, and the exponent numeric form may not be used. If the number of moles of each species is input in these columns the same restrictions apply, but an additional bit of information, an M in column 53, must

appear on the card. Column 53 is left blank for relative weights. Note that the relative weight and molar designations may not be mixed for any single problem.

The reactant enthalpy is placed in columns 54 to 62, and the units must be calories per mole. The number may appear anywhere in these columns, a decimal point must be used, and the exponent numeric form may not be used. A sign is required only if the enthalpy is negative. Obviously, this enthalpy must be consistent with the enthalpy base used for the THERMØ data. For the JANAF data, the enthalpy base is as follows: For each element, the phase, condensed or liquid, which is most stable at one atmosphere pressure is designated as a reference, or base, state. The heat of formation of this state at 298.15°K is arbitrarily specified as zero. Then all thermodynamic properties for other phases of the element, as well as for any compound containing the element, are referenced to the base state.

The initial state for each reactant is indicated by an S for solid, an L for liquid, or a G for gas in column 63. The initial reactant temperature, in degrees Kelvin, goes in columns 64 to 71. Both the initial state and temperature are used only to label the output printout and if they are omitted or input incorrectly, the calculations are not affected.

For all problem types (see Section IV.4) except a detonation problem, columns 73 to 79 are reserved for the reactant density in grams per cubic centimeter. The inputting of this data is optional, but if it is given, a decimal point must be used. For a detonation problem, columns 73 to 80 are used for the reactant specific heat at constant pressures. This data is required for each reactant for a detonation problem.

### 3. ØMIT/INSERT DATA

The purpose of the ØMIT/INSERT option is as follows. The program considers as possible products all species in the THERMØ data which are consistent with the chemical system which was input on the REACTANTS cards. Occasionally, it may be desired to eliminate one or more species from consideration as possible products. This may be accomplished by placing the species chemical formula on an ØMIT card. Both gaseous and condensed species may be omitted.

Only the names of condensed species may appear on an INSERT card. The INSERT option has been included for two reasons. The less important of the two is that if it is known beforehand that one or more particular condensed species will be among the final equilibrium composition for the first assigned point (i.e., the combustion chamber for a rocket problem), then a small amount of computer time can be saved by using an INSERT card. The more important reason for the INSERT option is that, in rare instances, it is impossible to obtain convergence without the use of an

INSERT card. This occurs when, by considering gases only, the temperature becomes extremely low. When this happens, the program outputs the following message: "LOW TEMPERATURE IMPLIES CONDENSED SPECIES SHOULD HAVE BEEN INCLUDED ON AN INSERT CARD" and no solution will be obtained. The user should resubmit the problem with one or more appropriate condensed species listed on an INSERT card.

The use of OMIT and INSERT cards is completely optional; however when used, each card must contain either the code word OMIT in columns 1 to 4 or INSERT in columns 1 to 6 and the chemical formulas of from one to four product species. The names of the species must be left-adjusted and begin in columns 16, 31, 46, or 61. In addition, the species name must be punched on the card exactly as it appears in the THERMO data. This means that the order of the chemical elements within the species name, the formula numbers, and the state of the species must all be identical. For example, gaseous ammonia would commonly appear as  $\text{NH}_3$ . Because of the alphabetizing scheme used for thermodynamic data, this species is written as H3N1(G).

#### 4. NAMELISTS DATA

The word NAMELIST is a FORTRAN IV statement and provides a convenient way of inputting data. One of the major advantages of the NAMELIST input method is that the data can be placed in any order and need not be placed within pre-specified card columns as is the case for the REACTANTS data. A secondary advantage is that the variable name appears with its numerical value on a card, thus making it easy to tell the purpose of each piece of data without having to refer to a program manual or to the program listing. Even though inputting data by means of NAMELIST is convenient, the following rules must be observed.

All data input by means of a NAMELIST statement must be associated with a NAMELIST name, and for this program there are only two: INPT2 and RKTINP. The first column of all NAMELIST data cards may not be used and must be blank. The second column of the first card only must contain a \$ character. The applicable NAMELIST name must be placed on the first card only. The name must begin in column 3, and must be followed by at least one blank column.

Each NAMELIST name is assigned a group of FORTRAN variables. (The variables belonging to INPT2 and RKTINP are listed in Tables V and VI, respectively.) These variables are assigned to a NAMELIST name within the program, and numeric data can only be input in conjunction with a NAMELIST name.

Although, in general, there are seven forms that input data may take, only three are of interest for this report. These are integer constants,

real number constants, and logical constants. These are defined as follows:

- a. An integer consists of one to eleven digits written without a decimal point.
- b. A real number constant may be written in two ways. The first form is from one to nine digits, including a decimal point, followed by an exponent. The exponent is written as the letter E followed by a sign and a one or two digit integer. For example 12345. could be written as 1.2345E04 or .12345+5, etc. The second form is one to nine digits, including a decimal point, but not followed by an exponent.
- c. A logical constant may be either true or false. There are two forms in which the constant may be written. These are either .TRUE. or T .FALSE. or F. The periods before and after the long forms are mandatory.

Logical constants may be associated only with logical variables. Integer constants may be associated with real variables and vice versa, and the proper conversion is made automatically by the computer. Note that when inputting data without a NAMELIST statement this conversion may cause difficulties and should only be used with great care.

On a NAMELIST card, each piece of data must be written in conjunction with its variable name (e.g., P = 100; or INDEX = 3, or PSIA = .TRUE., etc.). The equal sign is mandatory, and the data items must be separated by commas. If more than one card is required, the last item on each card, except for the last card, must be a constant followed by a comma. A variable name may not be the last item on the card. The end of a group of data is signaled by a \$ character. This may be on the same card as that containing the NAMELIST name if only one card is used or may be on any succeeding card, but it may not be the first character on a succeeding card. Note that it is not necessary to completely fill a card with data before beginning a subsequent card. In fact, the user may want to put each piece of data on separate cards. This facilitates subsequent data changes. One final note, it is not necessary to input data for every variable contained in a NAMELIST; however, each variable has been assigned a value within the program, and this value is used unless superseded by input data. The assigned values for all NAMELIST variables in this program are included in Tables V and VI.

To illustrate the preceding instructions, the following paragraphs discuss the specific NAMELIST data required by this program, what each data bit does, and then some specific examples.

The INPT2 NAMELIST data must be used for all problems. The variables in the INPT2 NAMELIST are listed and defined in Table V along with the type and assigned value of each variable. The type of problem (one of either TP, HP, RKT, or DETN), at least one pressure (P), and the relative amounts of fuel and oxidizer (i.e., one of either EQRAT, OF, FPCT, or FA) are required for each problem. The other variables are either completely optional or may be required only if a particular problem type is requested.

The variable JANF is a flag to indicate which thermodynamic data polynomial should be used. JANF=0 designates a polynomial of the form  $C_p = A_1 + A_2T + A_3T^2 + A_4T^3 + A_5T^4$ . This is the form used by the Lewis Research Center and is also the form the Armament Laboratory uses after converting the JANAF data.

The Lewis program is quite flexible in the type of problems it will consider or the thermodynamic variables which may be fixed. For gun propellant problems, it is most advantageous to assign the enthalpy and pressure which, in system nomenclature, constitutes an RKT problem.

#### a. RKT Problem

If RKT = .TRUE. or T, then a rocket problem is solved. A rocket problem is one for which the combustion takes place at an assigned enthalpy (REACTANTS cards) and assigned pressure (single value in the P variable), followed by an isentropic expansion. The combustion temperature, the thermodynamic properties and rocket performance are calculated for the chamber, the throat, and assigned exit points. The exit points desired are specified in the RKTINP namelist. If a temperature is assigned (T variable), then combustion will be assumed to occur at that temperature and not at the assigned enthalpy. The RKT problem type combines the H,S and T,S problems of the earlier program version. Note that, when this option is selected, the second set of NAMELIST data, RKTINP, is then required. The combustion gas conductivity and viscosity are computed for this option only.

#### b. DETN Problem

If DETN = .TRUE. or T, then the program solves a Chapman-Jouget detonation problem. The thermodynamic properties and composition downstream of the detonation wave are calculated for an assigned pressure and temperature upstream of the wave. This detonation calculation is primarily oriented for gas phase detonations. It is of limited utility for computation of detonations in solids, as the specific heat polynomial of the reactants must be on the data tape, which will not, in general, be the case for a typical solid explosive constituent ingredient.



c. P, PSIA, and MMHG Variables

The value P may be either the combustion pressure of a rocket engine (RKT problem) or a pressure at which composition and thermodynamic properties (TP or HP problem) are desired. Up to 26 values may be input, but only one is permitted for an RKT problem. The program assumes that the units of the pressures are in atmospheres unless either PSIA or MMHG are set true. If PSIA = .TRUE. or T then the pressure units are assumed to be in psia units. If MMHG = .TRUE. or T then the pressure units are assumed to be in millimeters of mercury. PSIA and MMHG may not both be set true in the same problem.

d. T Variable

Values for the T variable should be input only if TP is set true or if an assigned chamber temperature is desired for RKT problem. The temperature units must be degrees Kelvin.

e. EQRAT, ØF, FPCT, and FA Variables

The relative amounts of total fuel and total oxidizer may be expressed in one (and only one for each problem) of four ways. The mixture ratio (ØF) and percent fuel (FPCT) are self evident. The fuel-to-air weight ratio (FA) and equivalence ratio (EQRAT) are new to this version of the program and are not of use for gun propellant calculations.

f. IDEBUG Variable

If IDEBUG = .TRUE. or T then a printout of the intermediate calculation details is obtained. This is intended primarily as a debugging aid in the event there are problems. The output is extensive and is explained on page 34 of Reference 1.

g. IØNS Variable

If IØNS = .TRUE. or T then the program will consider ionized species. The earlier Lewis program version could not handle ionic species although provision was made in one of the subroutines for future consideration of ions. This capability is included in the newer program and thermodynamic data for ionized species are available as well as a sample problem which uses IØNS = T.

h. EQL, FRØZ, PCP, SUBAR, and SUPAR Variables

The five RKTINP variables (EQL, FRØZ, PCP, SUBAR, and SUPAR) in the RKTINP namelist are listed in Table VI. Of these, only PCP is required. The RKTINP namelist is required only if RKT is set true in the INPT2 namelist.

#### (1) PCP Variable

The value PCP is the ratio of the chamber pressure to the exit pressure. This is one of the independent variables (along with the entropy) for the nozzle portion of a rocket problem, and as such, at least one value must be input. As many as 22 values may be input; however, unlike the older program, values for the chamber and throat should not be input. Pressure ratios for the subsonic portion of the nozzle may be used. Values must be ordered so that the magnitudes increase monotonically.

#### (2) SUBAR and SUPAR Variables

Gun propellant performance at specific area ratios corresponding to a given gas velocity, either subsonic or supersonic, may be requested. Subsonic ratios are read as SUBAR and supersonic as SUPAR. When assigned area ratios are requested, the range of PCP values should be large enough to include the assigned area ratios. If the range is not large enough, extrapolation may be performed. SUBAR values should be ordered such that the values decrease and the SUPAR data should increase. Thirteen of each variable are permitted. Note that the use of this program feature is completely optional.

#### (3) EQL and FRØZ Variables

The program will calculate performance for both equilibrium and frozen expansions unless instructed otherwise. If EQL = .FALSE. or F then the equilibrium expansion is omitted and only frozen performance is calculated. If FRØZ = .FALSE. or F then the frozen expansion is omitted and only equilibrium performance is calculated.

TABLE V. VARIABLES IN INPT2 NAMELIST			
Variable Name	Variable Type	Value (Unless Set Differently)	Definitions
JANF	Integer	1.	Thermodynamic data polynomial indicator
P	Real	0.	Assigned pressures
T	Real	0.	Assigned temperatures
EQRAT	Real	0.	Equivalence ratio
ØF	Real	0.	Oxidant-to-fuel weight ratio
FPCT	Real	0.	Percent fuel by weight
FA	Real	0.	Fuel-to-air weight ratio
TP	Logical	False	Assigned temperature and pressure problem
HP	Logical	False	Assigned enthalpy and pressure problem
RKT	Logical	False	Rocket problem
DETN	Logical	False	Detonation problem
PSIA	Logical	False	Assigned pressure-to be in psia units
MMHG	Logical	False	Assigned pressures in millimeter of mercury units
IØNS	Logical	False	Consider ionic species
IDEBUG	Logical	False	Print intermediate output

TABLE VI. VARIABLES IN RKTNP NAMELIST			
Variable Name	Variable Type	Value Unless Set Differently	Definition
EQL	Logical	True	Gun propellant performance assuming equilibrium composition to be calculated
FRQZ	Logical	False	Gun propellant performance assuming frozen composition to be calculated
PCP	Real	0.	Ratio of chamber pressure to exit pressure
SUBAR	Real	0.	Subsonic area ratios
SUPAR	Real	0.	Supersonic area ratios

Table VII contains the input data for several propellant performance cases, and the output is listed on Tables VIII through XI. These cases are respectively M-10 (Case 100), M-9 (Case 101), an HMX-rubber propellant system (Case 102), and an RDX-triamino-guanidine nitrate formulation (Case 106). A comparison of these data with experimental or independent theoretical solutions gives the following results.

Case 100				
	Tv	Fp	$\gamma$	Mw
Lewis	3312	366,548	1.22	25.1
Experimental	3034	346,180	1.23	24.2
Case 101				
Lewis	3853	394,180	1.17	27.2
Experimental	3840	396,840	1.20	26.5
Case 102				
Lewis	2566	377,584	1.28	18.9
Other Theoretical	2545	373,000	(--)	18.9
Case 106				
Lewis	2637	390,870	1.29	18.8
Other Theoretical	2647	391,000	(--)	18.8

The input data (Table VII) are discussed in the program writeup except that no OMIT or INSERT cards are used.

TABLE VII. INPUT DATA FOR SAMPLE GUN PROPELLANT PROBLEMS

3 1													
C 24.0	H 29.5	O 41.3	N 10.6	1.0	-643100.	298.	F						
C 12.0	H 11.0	N 1.0		.33	27600.	298.	O						
C 2.0	H 14.0	O 6.0	N 4.0	.67	-66300.	298.	O						
CASE 100 PROPELLANT IS M-10													
\$INPT2 JANF=0,P(1)=5000.,RKT=TRUE.,FPCT=98.,PSIA=TRUE.,\$													
\$RKTINP PCP(1)=1.2,1.4,1.6,2.0,3.0,4.0,5.0,10.0,68.0,FROZ=FALSE,\$													
4 1													
C 24.0	H 29.5	O 41.3	N 10.6	1.0	-643100.	298.	F						
C 3.0	H 5.0	O 9.0	N 3.0	.96	-85300.	298.	O						
C 12.0	H 11.0	N 1.0	N 4.0	.02	27600.	298.	O						
C 3.0	H 14.0	O 6.0		.02	-66300.	298.	O						
CASE 101 PROPELLANT IS M-9													
\$INPT2 JANF=0,P(1)=5000.,RKT=TRUE.,FPCT=58.,PSIA=TRUE.,\$													
\$RKTINP PCP(1)=1.2,1.4,1.6,2.0,3.0,4.0,5.0,10.0,68.0,FROZ=FALSE,\$													
2 1													
C 4.0	H 8.0	O 8.0	N 8.0	1.0	17900.	298.	O						
C 7.0	H 11.0	O .2	N .02	1.0	-5000.	298.	F						
CASE 102 PROPELLANT IS HMX RUBBER													
\$INPT2 JANF=0,P(1)=5000.,RKT=TRUE.,FPCT=15.,PSIA=TRUE.,\$													
\$RKTINP PCP(1)=1.2,1.4,1.6,2.0,3.0,4.0,5.0,10.0,68.0,FROZ=FALSE,\$													
3 1													
C 4.0	H 8.0	O 8.0	N 8.0	1.0	17900.	298.	O						
C 7.0	H 11.0	O .2	N .02	.88	-5000.	298.	F						
T 11.0				.12	0.	298.	F						
CASE 103 PROPELLANT IS HMX-RUBBER WITH TITANIUM ADDED													
\$INPT2 JANF=0,P(1)=5000.,RKT=TRUE.,FPCT=17.,PSIA=TRUE.,\$													
\$RKTINP PCP(1)=1.2,1.4,1.6,2.0,3.0,4.0,5.0,10.0,68.0,FROZ=FALSE,\$													
4 1													
C 2.0	H 5.0	O 1.0	N 3.0	.83	22500.	298.	F						
C 4.0	H 6.0	N 4.0		.17	52400.	298.	F						
C 3.0	H 6.0	O 6.0	N 6.0	.60	14900.	298.	O						
C 1.0	H 9.0	O 3.0	N 7.0	.40	-11500.	298.	O						
CASE 106 PROPELLANT IS RDX-TAG NITRATE													
\$INPT2 JANF=0,P(1)=5000.,RKT=TRUE.,FPCT=16.,PSIA=TRUE.,\$													
\$RKTINP PCP(1)=1.2,1.4,1.6,2.0,3.0,4.0,5.0,10.0,68.0,FROZ=FALSE,\$													

TABLE VIII. OUTPUT FOR CASE 100, M-10 PROPELLANT

[illegible]

TABLE VIII. Concluded

MOLE FRACTIONS													
CH <sub>4</sub>	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
CO	.40188	.39739	.40060	.39943	.39834	.39637	.39229	.38996	.38611	.37568	.33827	.00000	.00000
CO <sub>2</sub>	.13746	.14238	.13868	.14019	.14130	.14339	.14339	.13991	.13978	.16431	.20966	.00000	.00000
H	.00104	.00046	.00082	.00066	.00054	.00039	.00020	.00012	.00000	.00002	.00000	.00000	.00000
H <sub>2</sub>	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00000	.00000	.00000	.00000	.00000
H <sub>2</sub> O	.00016	.00066	.00013	.00011	.00009	.00007	.00004	.00002	.00002	.00001	.00000	.00000	.00000
NH <sub>3</sub>	.10392	.10883	.10739	.10664	.10781	.10990	.11415	.11753	.12044	.13101	.17615	.00000	.00000
N <sub>2</sub>	.23507	.23088	.23392	.23283	.23180	.22989	.22585	.22253	.21968	.20916	.16394	.00000	.00000
NO	.00003	.00003	.00003	.00003	.00003	.00003	.00002	.00002	.00002	.00002	.00002	.00000	.00000
N <sub>2</sub> O	.00005	.00001	.00004	.00002	.00002	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000
OH	.11974	.11983	.11978	.11980	.11982	.11984	.11986	.11987	.11987	.11987	.11989	.00000	.00000
ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .00005 FOR ALL ASSIGNED CONDITIONS	.00061	.00019	.00043	.00032	.00024	.00015	.00006	.00003	.00001	.00000	.00000	.00000	.00000
C													
C <sub>2</sub> H <sub>4</sub>	C <sub>2</sub> H <sub>6</sub>	C <sub>2</sub> H <sub>2</sub>	C <sub>2</sub> H <sub>4</sub>	C <sub>2</sub> H <sub>6</sub>	C <sub>2</sub> H <sub>2</sub>	C <sub>2</sub> H <sub>4</sub>	C <sub>2</sub> H <sub>6</sub>	C <sub>2</sub> H <sub>2</sub>	C <sub>2</sub> H <sub>4</sub>	C <sub>2</sub> H <sub>6</sub>	C <sub>2</sub> H <sub>2</sub>	C <sub>2</sub> H <sub>4</sub>	C <sub>2</sub> H <sub>6</sub>
NH <sub>2</sub>	NH <sub>2</sub>	NH <sub>2</sub>	NH <sub>2</sub>	NH <sub>2</sub>	NH <sub>2</sub>	NH <sub>2</sub>	NH <sub>2</sub>	NH <sub>2</sub>	NH <sub>2</sub>	NH <sub>2</sub>	NH <sub>2</sub>	NH <sub>2</sub>	NH <sub>2</sub>
NOTE: WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS													
VISCOSITY AND CONDUCTIVITY VALUES BASED ON 99.8 PERCENT OF GAS MIXTURE													



# CUM PROPELLANT PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

24

TABLE IX. Concluded

[illegible][illegible]

TABLE X. OUTPUT FOR CASE 102, HMX-RUBBER

THEORETICAL GUN PROPELLANT PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION												
PC = 5000.0 PSIA												
CASE 102 PROPELLANT IS HMX-RUBBER												
CHEMICAL FORMULA												
OXIDANT C	4.00000	H	6.00000	O	6.00000	N	8.00000					
FUEL C	7.00000	H	11.00000	O	.20000	N	.02000					
O/F= 5.5667 PERCENT FUEL= 15.0000 EQUIVALENCE RATIO= 2.7550 DENSITY= 0.0000												
								WT FRACTION	ENTHALPY	STATE	TEMP	DENSITY
								(SEE NOTE)	CAL/MOL		DEG K	G/CC
								1.00000	17900.000		298.00	-0.0000
								1.00000	-5000.000		298.00	-0.0000
CHAMBER												
PC/P	1.000	THROAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
P, ATM	340.2	187.0	1.019	1.200	1.400	2.000	3.000	4.000	5.000	10.000	60.000	
T, CP, DEG K	1995	1758	1918	263.5	243.0	212.6	170.1	113.4	68.05	34.02	5.003	
H, CAL/G	43.8	-73.8	6.3	-24.2	-49.8	-91.0	-160.9	-207.0	-241.0	-337.8	-557.9	
S, CAL/(G)(K)	2.4686	2.4686	2.4686	2.4686	2.4686	2.4686	2.4686	2.4686	2.4686	2.4686	2.4686	
M, VOL WT												
(OLV/DLP) T	18.902	19.006	18.925	18.950	18.976	19.030	19.163	19.284	19.392	19.796	21.091	
(OLV/DLP) P	-1.01474	-1.02159	-1.01644	-1.01815	-1.01982	-1.02299	-1.02975	-1.03507	-1.03932	-1.05817	-1.07938	
CP, CAL/(G)(K)	1.0946	1.1603	1.1127	1.1309	1.1409	1.1639	1.2631	1.3303	1.3876	1.7060	2.2655	
GAMMA (S)	.5308	.5951	.5452	.5607	.5769	.6103	.6929	.7693	.8383	1.3712	2.3570	
SON VEL, M/SEC	1.2863	1.2791	.2854	1.2837	1.2817	1.2769	1.2642	1.2531	1.2438	1.1703	1.1394	
MACH NUMBER	0.000	1.000	.538	1.000	1.006	1.006	.934	.903	.880	.809	.693	
VEL, FT/SEC	0.0	3253.6	1837.3	2476.8	2903.8	3484.2	4293.7	4752.8	5064.5	5862.9	7351.1	
VISC, G/CM-SEC	.000604	.000555	.000588	.000576	.000565	.000548	.000521	.000504	.000493	.000469	.000416	
C, CAL/G-SEC-K	.000391	.000357	.000380	.000371	.000364	.000351	.000331	.000317	.000307	.000285	.000249	
T, CV, DEG K	2566											
IMPETUS												
377584.												
CSLAR, FT/SEC												
CF	.703	.397	.535	.535	.628	.753	.928	1.027	1.095	1.267	1.591	
AT/AT	1.000	1.290	1.072	1.014	1.006	1.006	1.123	1.279	1.431	1.704	2.087	
IVAC, LB-SEC/LB	180.2	210.6	187.0	181.4	180.6	187.3	193.6	198.6	213.6	248.0	298.0	
I, LB-SEC/LB	101.1	97.1	76.9	90.3	108.3	138.5	147.7	157.4	162.2	182.2	228.8	

TABLE X. Concluded

MOLE FRACTIONS															
C(S)	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000	0.00000
CH3	.00003	.00001	.00002	.00002	.00001	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.07542
CH4	.00418	.00735	.00494	.00571	.00649	.00605	.00617	.01175	.01508	.01603	.02372	.02120	.02372	.02120	.02120
CO	.00002	.00490	.00490	.00595	.00595	.00595	.00595	.00595	.00595	.00595	.00595	.00595	.00595	.00595	.00595
CO2	.00566	.00741	.00608	.00650	.00693	.00780	.00892	.01194	.01363	.01363	.02277	.02277	.02277	.02277	.02277
C2H2	.00002	.00001	.00002	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001
C2H4	.00002	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001
H	.00005	.00001	.00003	.00002	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001
HCN	.00136	.00074	.00114	.00098	.00085	.00067	.00043	.00030	.00023	.00023	.00023	.00023	.00023	.00023	.00023
HCO	.00007	.00002	.00005	.00004	.00003	.00002	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001	.00001
H2	.34336	.33076	.34237	.34127	.34009	.33764	.33162	.32616	.32141	.32141	.30765	.28640	.30765	.28640	.28640
H2O	.02193	.02248	.02165	.02165	.02210	.02266	.02413	.02545	.02656	.02656	.03329	.05793	.03329	.05793	.05793
NH3	.00065	.00056	.00062	.00060	.00057	.00054	.00049	.00045	.00042	.00042	.00042	.00042	.00042	.00042	.00042
N2	.21627	.21762	.21606	.21704	.21742	.21814	.21962	.22129	.22259	.22259	.22518	.22518	.22518	.22518	.22518
ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .00005 FOR ALL ASSIGNED CONDITIONS															
C	CH	CH2	CN	CN2	C2	C2H	C2H2	C2H4	C2H6	C2N2	C2O	C2O2	C2O4	C2O6	C2O8
C3	H2O2	H2O2L	H2O2S	N	NH	NH2	NH3	NH4	NH5	NH6	NH7	NH8	NH9	NH10	NH11
N2H4	N2O	N2O2	O	OH	O2	O3	O4	O5	O6	O7	O8	O9	O10	O11	O12
NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS															
VISCOSITY AND CONDUCTIVITY VALUES BASED ON 99.4 PERCENT OF GAS MIXTURE															

TABLE XI. OUTPUT FOR CASE 106, RDX-TRIAMINO GUANIDINE NITRATE

~~THEORETICAL GUN PROPELLANT PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION~~

PC = 500.0 PSIA

CASE 136      PROPELLANT IS ROX-TAG NITRATE

CHEMICAL FORMULA		Wt FRACTION	ENTHALPY	STATE	TEMP	DENSITY
		(SEE NOTE)	CAL/MOL		DEG K	G/CC
FUEL	C 2.000000 H 5.000000 O 1.000000	N	3.000000		298.00	-0.00000
FUEL	C 4.000000 H 6.000000 O 4.000000	N	6.000000		298.00	-0.00000
OXYDANT	C 3.000000 H 6.000000 O 6.000000	N	7.000000		298.00	-0.00000
OXYDANT	C 1.000000 H 9.000000 O 3.000000	N	7.000000		298.00	-0.00000

0/F=	2.3333	PERCENT FUEL=	30.0000	EQUIVALENCE RATIO=	2.6026	DENSITY=	0.0000
------	--------	---------------	---------	--------------------	--------	----------	--------

[illegible][illegible]

## HOLE FRACTIONS

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .000005 FOR ALL ASSIGNED CONDITIONS

~~NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS~~

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TABLE XII. THERMO DATA INPUT FORMAT FOR TITANIUM DIOXIDE

-62000.0	9	51	TITANIUM DIOXIDE (TiO2) IDEAL GAS									
298	300	400	500	600	700	800	900	1000				
10.838	10.858	11.820	12.548	13.079	13.464	13.746	13.957	14.117				
0.000	.020	1.156	2.376	3.659	4.987	6.348	7.734	9.138				
56.146	56.213	59.474	62.194	64.531	66.578	68.395	70.027	71.506				
1000	1100	1200	1300	1400	1500	1600	1700	1800	1900	2000	2100	2200
3000	3100	3200	3300	3400	3500	3600	3700	3800	3900	4000	4100	4200
5000	5100	5200	5300	5400	5500	5600	5700	5800	5900	6000		
14.117	14.211	14.339	14.417	14.480	14.532	14.575	14.611	14.641	14.667			
14.690	14.709	14.725	14.741	14.754	14.765	14.776	14.785	14.793	14.800			
14.807	14.813	14.819	14.824	14.828	14.832	14.836	14.840	14.843	14.846			
14.849	14.852	14.854	14.856	14.858	14.860	14.862	14.864	14.866	14.867			
14.869	14.870	14.871	14.872	14.874	14.875	14.876	14.877	14.878	14.878			
14.879												
9.138	10.556	11.985	13.423	14.868	16.319	17.774	19.234	20.696	22.162			
23.630	25.099	26.571	28.045	29.519	30.995	32.472	33.950	35.429	36.909			
38.389	39.870	41.352	42.834	44.317	45.800	47.283	48.767	50.251	51.736			
53.220	54.705	56.191	57.676	59.162	60.648	62.134	63.620	65.107	66.593			
68.080	69.567	71.054	72.541	74.029	75.516	77.004	78.491	79.979	81.467			
82.955												
71.506	72.858	74.101	75.252	76.323	77.324	78.263	79.147	79.948	80.776			
81.529	82.246	82.931	83.586	84.213	84.816	85.395	85.953	86.491	87.010			
87.512	87.997	88.468	88.924	89.336	89.796	90.214	90.621	91.017	91.402			
91.778	92.145	92.503	92.852	93.194	93.528	93.854	94.174	94.487	94.794			
95.094	95.383	95.677	95.960	96.238	96.511	96.779	97.043	97.301	97.556			
97.806												

TABLE XIII. THERMO DATA OUTPUT FORMAT FOR TITANIUM DIOXIDE

## TITANIUM DIOXIDE (TiO2) IDEAL GAS

HO = -62000.0

VALUES OF G  
COEFFICIENTS ARE

36725340E+01	10003020E-01	11120307E-04	49403359E-08	67934354E-12	32588921E+05	79567663E+01
--------------	--------------	--------------	--------------	--------------	--------------	--------------

-33589155E-02	-54917462E-02	-15152376E-01				
---------------	---------------	---------------	--	--	--	--

T	CP	CCP	HT	CHT	ST	GST	DCP	DHT	DST
---	----	-----	----	-----	----	-----	-----	-----	-----

298.	10.838	10.838	0.000	0.100	56.146	56.146	.000	0.000	.000
300.	10.850	10.866	.020	.022	56.213	56.219	.002	.002	.006
400.	11.820	11.816	1.156	1.158	59.474	59.480	.004	.002	.006
500.	12.540	12.540	2.376	2.377	62.194	62.194	.008	.001	.004
600.	13.079	13.076	3.659	3.659	64.531	64.534	.003	.000	.003
700.	13.464	13.465	4.987	4.987	66.578	66.581	.001	.000	.003
800.	13.746	13.746	6.348	6.349	68.395	68.398	.000	.001	.003
900.	13.957	13.958	7.734	7.734	70.027	70.030	.004	.000	.002
1000.	14.117	14.118	9.138	9.138	71.506	71.509	.001	.000	.003

VALUES OF G  
COEFFICIENTS ARE

62406076E+01	12046967E-02	-50104624E-06	.85525393E-10	-.53125222E-14	-.32336518E+05	-.01070897E+01
--------------	--------------	---------------	---------------	----------------	----------------	----------------

95760211E-01	22837632E-01	10773479E+00				
--------------	--------------	--------------	--	--	--	--

T	CP	CCP	HT	CHT	ST	GST	DCP	DHT	DST
---	----	-----	----	-----	----	-----	-----	-----	-----

1000.	14.117	14.117	9.138	9.138	71.506	71.506	.000	.000	.000
1100.	14.241	14.214	10.556	10.555	72.858	72.856	.027	.001	.002
1200.	14.339	14.301	11.985	11.981	74.101	74.097	.038	.004	.004
1300.	14.417	14.379	13.423	13.415	75.252	75.245	.038	.008	.007
1400.	14.480	14.447	14.868	14.856	76.323	76.313	.033	.012	.010
1500.	14.532	14.508	16.319	16.304	77.324	77.312	.024	.015	.012
1600.	14.575	14.561	17.774	17.757	78.263	78.250	.014	.017	.013
1700.	14.611	14.607	19.234	19.216	79.147	79.134	.004	.018	.013
1800.	14.641	14.646	20.696	20.678	79.948	79.970	.005	.018	.022
1900.	14.667	14.681	22.162	22.145	80.776	80.763	.014	.017	.013
2000.	14.690	14.709	23.630	23.614	81.529	81.516	.019	.016	.013
2100.	14.709	14.734	25.099	25.086	82.246	82.235	.025	.013	.011
2200.	14.726	14.754	26.571	26.561	82.931	82.921	.028	.010	.010
2300.	14.741	14.771	28.046	28.037	83.586	83.577	.030	.008	.009
2400.	14.754	14.784	29.515	29.515	84.213	84.206	.030	.004	.007
2500.	14.765	14.795	30.985	30.984	84.816	84.809	.030	.001	.007
2600.	14.776	14.803	32.472	32.474	85.395	85.390	.027	.002	.005
2700.	14.785	14.808	33.968	33.964	85.953	85.949	.024	.004	.004
2800.	14.793	14.814	35.429	35.435	86.491	86.487	.021	.006	.004
2900.	14.800	14.817	36.909	36.917	87.010	87.007	.017	.008	.003
3000.	14.807	14.819	38.389	38.399	87.512	87.510	.012	.010	.002
3100.	14.813	14.821	39.870	39.881	87.997	87.995	.008	.011	.002
3200.	14.819	14.821	41.352	41.363	88.468	88.466	.002	.011	.002
3300.	14.824	14.822	42.834	42.845	88.924	88.922	.002	.011	.002
3400.	14.828	14.823	44.317	44.327	89.336	89.365	.005	.010	.029
3500.	14.832	14.823	45.800	45.810	89.796	89.794	.009	.010	.002
3600.	14.836	14.824	47.283	47.292	90.214	90.212	.012	.009	.002
3700.	14.840	14.825	48.767	48.775	90.621	90.618	.015	.008	.003
3800.	14.843	14.827	50.251	50.257	91.017	91.013	.016	.006	.004
3900.	14.846	14.829	51.736	51.740	91.402	91.399	.017	.004	.003
4000.	14.849	14.832	53.220	53.220	91.778	91.774	.017	.003	.004
4100.	14.852	14.836	54.705	54.706	92.145	92.140	.017	.001	.005
4200.	14.854	14.839	56.191	56.198	92.503	92.498	.015	.001	.005
4300.	14.856	14.844	57.676	57.674	92.852	92.847	.012	.002	.005
4400.	14.858	14.848	59.162	59.159	93.194	93.188	.010	.003	.006
4500.	14.860	14.854	60.644	60.644	93.528	93.522	.006	.001	.006
4600.	14.862	14.859	62.134	62.130	93.854	93.849	.003	.004	.005
4700.	14.864	14.865	63.620	63.616	94.174	94.168	.001	.004	.006
4800.	14.866	14.871	65.107	65.103	94.487	94.481	.005	.004	.006
4900.	14.867	14.876	66.593	66.590	94.794	94.788	.009	.003	.006
5000.	14.869	14.881	68.080	68.078	95.094	95.089	.012	.002	.005
5100.	14.870	14.886	69.567	69.566	95.388	95.383	.016	.001	.005
5200.	14.871	14.889	71.054	71.055	95.677	95.672	.018	.001	.005
5300.	14.872	14.892	72.541	72.544	95.960	95.956	.020	.003	.004
5400.	14.874	14.893	74.029	74.033	96.238	96.235	.019	.004	.003
5500.	14.875	14.892	75.516	75.523	96.511	96.508	.017	.002	.003
5600.	14.876	14.889	77.004	77.012	96.779	96.776	.013	.008	.003
5700.	14.877	14.883	78.491	78.500	97.043	97.040	.006	.009	.003
5800.	14.878	14.875	79.979	79.988	97.301	97.298	.003	.009	.003
5900.	14.878	14.862	81.467	81.475	97.556	97.553	.016	.008	.003
6000.	14.875	14.847	82.955	82.960	97.806	97.802	.032	.005	.004



TABLE XIV. DATA TAPE FORM FOR THERMØ DATA OUTPUT

T102	J 6/70T1	10	200	000	06	299.000	6000.000	1
C.62406876E+01	0.12846967E-02	-0.50184624E-06	0.85525393E-10	-0.53125222E-14				2
-0.3336518E+05	0.81878897E+01	0.30725348E+01	0.10883020E-01	-0.11120307E-04				3
0.49483359F-08	-0.67934354F-12	-0.32508921E+05	0.79567663F+01					4

## SECTION V

### THERMO DATA PROGRAM

The program (Appendix II) to fit the tabular JANAF thermochemical data to the Lewis polynomial is relatively simple and straightforward. JANAF data for Cp, H, and S is read in the tabular form for two temperature ranges 298° to 1,000°K and 1,000° to 6,000°K. The format is as shown in Table XII for the gas  $\text{TiO}_2$ . The first line consists of the reference heat of formation to 298°K in calories per mole, the number of points in the first temperature range and the number of points in the second temperature range, followed by a species identifier. The tabular temperature references for the first interval are then listed followed by the appropriate Cp, H, and S values. This sequence is then repeated for the second temperature range. Subsequent to data input, the program establishes a matrix which it solves by an inversion procedure to obtain the required polynomial constants. These constants are then output in the form suitable for inclusion on the Lewis program thermodynamic data tape.

The output is as shown on Table XIII for the  $\text{TiO}_2$  species which is also shown on the input. The coefficients required on the data card for the first temperature range are shown on the first line followed by a comparison between the tabular data and the generated polynomials for the three functions of interest. It can be seen that the data fit is quite good. These data are followed by the required constants for the second temperature range and a similar comparison of polynomial and tabular results.

These results are read onto the data tape in the form shown on Table XIV. There are four cards per species. The first line consists of the empirical formula in columns 1 to 12. A gaseous species has no subscript, a liquid, has subscript L, and a solid, has subscript S. Columns 19 to 21 contain a code for the data source, in this case, a J for the JANAF tables. Columns 22 to 24 are the month and year of polynomial computation. The first through the fourth atoms in the species are inserted in columns 25 and 26, 30 and 31, 35 and 36, 40 and 41, while the respective number of atoms are placed in columns 27 to 29, 32 to 34, 37 to 39, and 42 to 44. Column 45 is used for the phase of the species G, L, or S. Columns 46 through 55 have the lower temperature bound at which the species exists with the upper temperature bound being placed in columns 56 through 65.

Cards 2, 3, and 4 contain the 14 polynomial constants, five each on cards 2 and 3 and four on card 4.

APPENDIX I  
LEWIS PROGRAM LISTING

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C	I E R P G	REFERENCE PROGRAM	ODE	P1712	00002
C	DECK SEQUENCED BY SUBROUTINE			P1712	00003
C	THERMODYNAMIC DATA FOLLOWS SOURCE DECK			P1712	00004
C	DATA FOR TEST CASES FOLLOWS THERMODYNAMIC DATA			P1712	00005
C	PROGRAM USES TAPE UNIT 4 FOR THERMO DATA			P1712	00006
C	ODE ICRPG REFERENCE PROGRAM			P1712	00007
C	MAIN PROGRAM			P1712	00008
C	UCUBLE PRECISION G.X			P1712	00009
C	INTEGER DATA, ORIT, ENSERT, REAC, BLANK, THRM, END, SUB			P1712	00010
C	LOGICAL HP, SP, TP, IDEBUG, NEMR, IONS, MOLES, FROZ, E3L, PSIA, RKT			P1712	00011
C	LOGICAL SHOCK, MPMG, PASCAL, EV, IC, DETN, CPCVFR, CPCVEG, SIUNIT, EUNITS			P1712	00012
C	DIMENSION OMIT(2,3), NCD(4), ENSERT(13,3), LH(2), LVP(2), LVM(2)			P1712	00013
C	COMMON/POINTS/HSUT(13), SSUM(13), CPR(13), DVTP(13), DULVPT(13)			P1712	00014
C	1, GAMHAS(13), P(26), T(26), V(13), PPP(13), MM(13), SONVEL(13), TIT(13)			P1712	00015
C	2, TOTN(13)			P1712	00016
C	COMMON/SPECES/CDEF(2,7,150), S(150), EN(150,13), ENLN(150), H3(150)			P1712	00017
C	1, CELN(150), A(15,150), SUB(150,3), IUSE(150), TEMP(50,2)			P1712	00018
C	COMMON/MISC/ENN, SUMN, IT, SO, ATOM(3,101), LLMT(15), 80P(15,2)			P1712	00019
C	1, TM, TLOW, THIU, TH15H, PP, CPSUM, OF, EQRT, FPCT, R, RR, RSUBU, AG(2), AM(2)			P1712	00020
C	2, HPP(2), RHU(2), VMIN(2), VPLS(2), MP(2), DATA(22), NAME(15,5)			P1712	00021
C	3, ANUM(15,5), PECHT(15), ENTH(15), FAZ(15), RTEHP(15), FOX(15), DENS(15)			P1712	00022
C	4, RHOP, KYM(15), LCN, JANF			P1712	00023
C	COMMON/DOUBLE/ G(20,21), X(20)			P1712	00024
C	COMMON/INDEX/ IDEBUG, CONVG, TP, HP, SP, HPSP, TPSP, MOLES, NP, NT, NPI, L, NS, XMAT, INAT, IGIN, J, NMOT, IP, NEMR, NSUB, NSUP, ITN, CPCVFR, CPCVEU			P1712	00025
C	2, IONS, NC, NSERT, JSOL, JULIQ, KASE(14), NREAC, IC, IO2			P1712	00026
C	COMMON/PERF/PCP(26), VRQC(13), SPIH(13), VAGI(13), SUBAR(13), SUPAR(13)			P1712	00027
C	1, CPRF(13), AEAT(13), CSTR, EGL, FROZ, SSO			P1712	00028
C	EQUIVALENCE (OMIT, ENLN), (ENSERT, EN(1,3))			P1712	00029
C	DATA MIT/4HOMIT/, BLANK/1H /, PSIA/4HPSIA/, REAC/4HREAC/.			P1712	00030
C	1, INPUT/4HINPUT/, IE/1HE/, INSERT/4HINSE/, THRM/4HTHER/, END/3HEND/			P1712	00031
C	DATA LH/4HL/, CA, 4HL/G /, LVP/2HJV+, 1H /, LVM/2HVM-, 1H /, NMLT/4HNMLT/			P1712	00032
C	NAMELIST/INPT2/JANF, P, T, EQRT, OF, F, PGI, F, A, TP, HP, SP, RKT			P1712	00033
C	1, PSIA, MPMG, SHOCK, IONS, EV, V, DETN, CPCVFR, CPCVEG, IDEBUG			P1712	00034
C	2, SIUNIT, EUNITS			P1712	00035
C	TLOW = 0.			P1712	00036
C	NEMR = .FALSE.			P1712	00037
C	DO 399 I=1,15			P1712	00038
C	DO 398 J=1,150			P1712	00039
C	A(I,J) = 0.0			P1712	00040
C	398 CONTINUE			P1712	00041
C	399 CONTINUE			P1712	00042
C				P1712	00043
C				P1712	00044
C				P1712	00045
C				P1712	00046
C				P1712	00047
C				P1712	00048
C				P1712	00049
C				P1712	00050
C				P1712	00051
C				P1712	00052
C				P1712	00053
C				P1712	00054



```

300 CONTINUE
    V1 = 0.
    V2 = 0.
    RHOP = 0.
    KASE = 0
    IP = .FALSE.
    HP = .FALSE.
    SP = .FALSE.
    RKT = .FALSE.
    CPCVR = .FALSE.
    CPCVEJ = .FALSE.
    SHOCK = .FALSE.
    DETN = .FALSE.
    EV = .FALSE.
    PASCAL = .FALSE.
    MMHG = .FALSE.
    PSIA = .FALSE.
    R = 1.987165
    TR = 418.7
    SIUNIT = .FALSE.
    EUNITS = .FALSE.
    IONS = .FALSE.
    IDEBUG = .FALSE.
    FA = 0.
    UF = 0.
    EGRAT = 0.
    FPCT = 0.
    EGL = .TRUE.
    READ(5,303)KASE
    303 FORMAT(13A5,A2)
    300(5,INPT2)
    DO 305 I=1,26
    IF(P(I).EQ.0.) GO TO 322
    NP = I
    IF (MMHG) P(NP) = P(NP)/760.
    IF (PASCAL) P(NP) = P(NP)/101325.
    IF(P(SI))
    7 P(NP)=P(NP)/14.596096
    305 CONTINUE
    322 IF (FA.NE.0.) OF = 1./FA
    IF(EORAT.EQ.0.) GO TO 725
    OF = (-EORAT*VMIN(2)-VPLS(2))/(VPLS(1)+EGRAT*VHIN(1))
    GO TO 727
    725 IF(OF.NE.0.) GO TO 727
    IF(FPCT.EQ.0.) GO TO 9051
    OF = (1.-FPCT)/FPCT
    GO TO 727
    9051 WRITE(6,724)
    724 FORMAT(48HNO INPT2 VALUE GIVEN FOR OF, EGRAT, FA, OR FPCT )
    727 WP(1) = OF
    WP(2) = 1.
    SUM = WP(1)+WP(2)
    FPCT = 100.*WP(2)/SUM

```

```
160 IF (EORAT.NE.0.) GO TO 745
    V2 = (WP(1)*VMIN(1)+WP(2)*VMIN(2))/SUM
    V1 = (WP(1)*VPLS(1)+WP(2)*VPLS(2))/SUM
    IF (V2.NE.0.) EORAT=ABS(V1/V2)
    745 DO 747 I=1,L
        80(I) = (WP(1)*BOP(I,1)+WP(2)*BOP(I,2))/SUM
    747 CONTINUE
    IF (EORAT.EQ.1.) EORAT= 1.000005
    IF (.NOT.IONS.OR.L.NI(L).EQ.IE) GO TO 748
    L = L+1
    LL*1(L) = IE
    80(L) = 0.
    748 HSUB0 = (WP(1)*HPP(1)+WP(2)*HPP(2))/SUM
    WRITE (6,INPT2)
    WRITE (6,752)KASE
    752 FORMAT(1H0,13A6,A2/)
    WRITE (6,770)
    770 FORMAT(1H0,17X,4HFUEL,13X,7HOXIDANT,12X,7HMIXTURE //)
    780 FORMAT(1H0,24X,SEIS=877)
    WRITE (6,790) LH,HPP(2),HPP(1),HSUB0,LVP,VPLS(2),VPLS(1),V1,
    1LVM,VMIN(2),VMIN(1),V2
    HSUB0 = HSUB0/R
    WRITE (6,785)
    785 FORMAT(8H ATOMS/G )
    RHOP = WP(2)*RH0(1)+WP(1)*RH0(2)
    IF (RHOP.NE.0.) RHOP = (WP(1)+WP(2))*RH0(1)*RH0(2)/RHOP
    795 IF (NEWR) CALL SEARCH
    701 = L+1
    IF (NC.EQ.0) GO TO 790
    80 302 J=1,NS
    IF (IUSE(J).EQ.0) GO TO 302
    IF (IUSE(J).GT.0) IUSE(J) = -IUSE(J)
    IF (INSERT.EQ.0) GO TO 302
    00 301 I=1,MSERT
    IF (SUB(J,1).NE.INSERT(1,I)) GO TO 301
    IF (SUB(J,2).NE.INSERT(2,I)) GO TO 301
    IF (SUB(J,3).NE.INSERT(3,I)) GO TO 301
    INSERT(1,I) = 0.
    IQ1= I01+1
    IUSE(J) = -IUSE(J)
    301 CONTINUE
    302 CONTINUE
    NSERT = 1
    790 IIN= 35
    IC = .FALSE.
    PP = NS
    NPT = 1
    ENN = 1
    SUPN = ENN
    XI = NS - NC
    XI = ENN/XI
    XLN = AL9G(XI)
```

```

215      UU 432 J=I,NS
          IF(IUSE(J),50,-10000) IUSE(J)=0
          EN(J,1) = 0,
          ENLN(J)=0,
          IF (IUSE(J),NE,0) GO TO 432
          EN(J,1) = XI
          ENLN(J) = XLN
220      432 CONTINUE
          JSCL = 0
          JLIQ = 0
          IF(OETN) CALL DETON
          IF(RKT) CALL ROCKET
          IF (TP) CALL HOLIER
          IF (WP) CALL CMBSYN
          500 CONTINUE
              GC TO 1
              END
225
```

P1712 00214  
P1712 00215  
P1712 00216  
P1712 00217  
P1712 00218  
P1712 00219  
P1712 00220  
P1712 00221  
P1712 00222  
P1712 00223  
P1712 00224  
P1712 00225  
P1712 00226  
P1712 00227  
P1712 00228  
P1712 00229  
P1712 00230





[illegible]



## SUBROUTINE CPHS

COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),HQ(150)

1 .GELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)

COMMON/SC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),80(15),80P(15,2)

1 .TM, .OK,THID,THIGH,PP,CPSUM,OF,FOUR,FPCT,R,R,HSUB0,AC(2),AM(2)

2 .PPPT(27),RHOT(27),VPLST(27),VPLST(27),DATA(27),NAME(15,5)

3 .ANUM(15,5),PECT(15),ENTH(15),FAZ(15),RTMP(15),FOX(15),DENS(15)

4 .RHOP,RMH(15),TLN,JANF

COMMON/INDEX/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,L,NS,

1 .KNAT,THAT,IQ1,N,J,NOHIT,IP,NEHR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ

2 .IONS,NC,NSERT,JSOL,JIQ,ICASE(14),NREAG,IC,IQ2

K = 1

IF (TT.LF.TMID)K = 2

KK = 0

CPSUM=0.

90 IF (COEF(K,1,J).NE.0.)GO TO 97

IF (IUSE(J).LT.0) GO TO 100

KK = K

K = 1

IF (KK.EQ.1) K = 2

97 CONTINUE

IF (JANF.EQ. 0)GO TO 98

S(J)=COEF(K,1,J).TLN+COEF(K,7,J).TLN+COEF(K,5,J)/2./TT/TT

1+(COEF(K,4,J)/3.0+TT+COEF(K,3,J)/2.0)\*TT+COEF(K,2,J))\*TT

HQ(J)=((COEF(K,4,J)/4.0)\*TT+COEF(K,3,J)/3.0)\*TT+COEF(K,2,J))\*TT

1TT+COEF(K,1,J)-(COEF(K,5,J)/TT-COEF(K,6,J))/TT

CPSUM=CPSUM ((COEF(K,4,J)\*TT+COEF(K,3,J))\*TT+COEF(K,2,J))\*TT

1+COEF(K,1,J)-COEF(K,5,J)/TT/TT)\*EN(J,NPT)

GO TO 99

98 S(J) = (((COEF(K,5,J)/4.)\*TT+ COEF(K,4,J)/3.)\*TT+ COEF(K,3,J)/2.

1)\*TT+COEF(K,2,J))\*TT+ COEF(K,1,J)\*TLN + COEF(K,7,J)

HQ(J) = (((COEF(K,5,J)/5.)\*TT+ COEF(K,4,J)/4.)\*TT+ COEF(K,3,J)/3.

1)\*TT+ COEF(K,2,J)/2.)\*TT+ COEF(K,1,J) + COEF(K,6,J)/TT

CPSUM= CPSUM+(((COEF(K,5,J)\*TT+ COEF(K,4,J))\*TT+ COEF

1)\*TT+COEF(K,2,J))\*TT+COEF(K,1,J))\*EN(J,NPT)

99 CONTINUE

IF (KK.EQ.0) C. TO 100

K = KK

KK = 0

100 IF (J.EQ.NS) GO TO 200

J=J+1

GO TO 90

200 RETURN

ENC

SUBROUTINE DETON									
C	C					P1712	00401		
C	C					P1712	00402		
C	C					P1712	00403		
C	C					P1712	00404		
05	C					P1712	00405		
	C					P1712	00406		
	C					P1712	00407		
	C					P1712	00408		
	C					P1712	00409		
10	C					P1712	00410		
	C					P1712	00411		
	C					P1712	00412		
	C					P1712	00413		
	C					P1712	00414		
15	C					P1712	00415		
	C					P1712	00416		
	C					P1712	00417		
	C					P1712	00418		
	C					P1712	00419		
20	C					P1712	00420		
	C					P1712	00421		
	C					P1712	00422		
	C					P1712	00423		
	C					P1712	00424		
25	C					P1712	00425		
	C					P1712	00426		
46	C					P1712	00427		
	C					P1712	00428		
	C					P1712	00429		
30	C					P1712	00430		
	C					P1712	00431		
	C					P1712	00432		
	C					P1712	00433		
35	C					P1712	00434		
	C					P1712	00435		
	C					P1712	00436		
	C					P1712	00437		
	C					P1712	00438		
	C					P1712	00439		
40	C					P1712	00440		
	C					P1712	00441		
	C					P1712	00442		
	C					P1712	00443		
45	C					P1712	00444		
	C					P1712	00445		
	C					P1712	00446		
	C					P1712	00447		
	C					P1712	00448		
50	C					P1712	00449		
	C					P1712	00450		
	C					P1712	00451		
	C					P1712	00452		
	C					P1712	00453		

```

55 7 IF (AM(1).NE.0.0) AND. AM(2).NE.0.0) GO TO 4
    AM1 = AM(2)
    IF (AM(2).EQ.0.0) AM1 = AM(1)
    GO TO 9
    4 AM1 = (MP(1)+MP(2))*AM(1)*AM(2)/(MP(2)*AM(1)+MP(1)*AM(2))
    3 CONTINUE
    60 DO 902 IT=1,NT
        TI = T/IT
        IF (CALCH) CALL HCALC
        CP1 = (MP(1)*AC(1)+MP(2)*AC(2))/(MP(1)+MP(2))
        DO 902 IP=1,NP
            PI = P/IP
            H1(NPI) = HSUB0
            TUB(NPI)=TI
            PUR(NPI)=PI
            CP(NPI) = CP1*P
            ITR= 0
            IT= 3000.
            PP1= 15.
            PP= PP1*PI
            HSUB0 = H1(NPI)/R + .75*TI*PP1/AM1
            TP = .FALSE.
            HP = .TRUE.
            CALL EOLDRM
            HSUB0 = H1(NPT)
            MP= .FALSE.
            IF (TI.EQ.0.) GO TO 1000
            GAP= GAMMAS(NPT)
            TI1= TI/TI
            II= 0
            TEM=TI1-.75*PP1/(CPR(NPT)*AM1)
            AM=MH(NPT)/AM1
            IF (IDEBUG) WRITE(6,190)
            190 FORMAT(33HDETONATION VELOCITY CALCULATIONS /11X,4HP/PI,17X,4HT/11
                1)
            IF (IDEBUG) WRITE(6,203) II,PP1,TI1
            C
            200 DO 202 II=1,4
                ALFA=AMH/TI1
                PP1= (1.+GAM)* (1.+(1.-G.*GAM*ALFA/(1.+GAM))*2)**.5)/(2.*GAM*.LFA)
                RK=PP1*ALFA
                TIT= TEM+.5*PP1*GAM*(RK*RK-1.)/(AM1*CPR(NPT)*RK)
                IF (IDEBUG) WRITE(6,203) II,PP1,TI1
                203 FORMAT(15,2E20.8)
                202 CONTINUE
                TP= .TRUE.
                IT= TI*TI1
                AM1 = PP1*AMH/TI1
            C
            205 ITR= ITR+1
            PP= PP1*PP1
            CALL EOLDRM

```

```
IF (NPT.EQ.0) GO TO 1000
*F (TT.EQ.0) GO TO 860
GAM= GAMAS(NPT)
IF (CPCVFR) GAM= CPRF(NPT) / (CPRF(NPT)-1./WM(NPT))
IF (CPCVEU) GAM= -GAMAS(NPT)*DLVPT(NPT)
AMP= AM(NPT)/AM1
KRI= PP1*AM/TT1
A11= 1./PP1 + GAM*RR1*DLVPT(NPT)
A12= GAM*RR1*DLVTP(NPT)
A21= .5*GAM*(RR1**2-1.-DLVPT(NPT)*(1.+RR1**2))*DLVTP(NPT)-1.
A22= -.5*GAM*DLVTP(NPT)*(RR1**2+1.-WM(NPT)*CPR(NPT))
B1= 1./PP1-1.*GAM*(RR1-1.)
B2= WM(NPT)*(RSUM(NPT)-HI(NPT)/R)/TT-.5*GAM*(RR1*RR1-1.)
X1= XX(Y)
X2= YY(Z)
ALAM= 1.
TE4= X1
IF (TEM.LI.0.) TEM= -TEM
IF (X2.GT.TEN) TEN=X2
IF (-X2.GT.TEN) TE4= -X2
IF (TEM.GT.0.4) ALAM=.4/TEM
PP1= PP1*EXP(X1*ALAM)
TT1= TT1*EXP(X2*ALAM)
TT= TT1*TT1
US= (RR*GAM*TT/WM(NPT))**.5
UD= RR1*UG
IF (IDERUG) WRITE(6,10) ITR
10 FORMAT (21H0 ITERATION NUMBER=I2 )
IF (IDERUG) WRITE(6,30) PP1,TT1,RR1,X1,X2,US
30 FORMAT (6X,4HP/PI,10X,1H= E20.8/6X,4HT/TT, 10X,1H= E20.8/6X,8HRH0/R0
101.6X,1H= E20.8/6X,11HDEL IN P/PI,3X,1H=E20.8/6X,11HDEL IN T/TT,3X
2.1H=E20.8/6X,2HUS,12X,1H=E20.8)
CONVERGENCE TEST
IF (ITR.LE.10 .AND. TEM.GT.0.5E-04) GO TO 205
KRM(NPT)=RR1
IF (CP(NPT).EQ.0.) GO TO 40
GM1(NPT)= CP(NPT) / (CP(NPT)-R/AM1)
VMCC(NPT)= UD/RR*GM1(NPT)*T1/AM1**.5
GO TO 41
40 GM1(NPT)= 0.
VMCC(NPT)= 0.
GO TO 150
150
C
C DERIVATIVES
41 IF (IDERUG) WRITE(5,55)
55 FORMAT (17H0 DERIVATIVE OF:13X,AMEN P,10X,AMEN T,10X,2HUD,
1
/3X,2HBY )
B1= 1./PP1-GAM*RR1
B2= GAM*RR1**2
X1= XX(Y)
```

```
160 X2 = YY(2)
    AA = .5*(1.-OLVPT(NPT))
    88 = .5*OLVPT(NPT)
    OUC = UD*(AA*X1+BB*X2-1.)
    X1 = X1-1.0
165 IF(IDERUG) WRITE(6,81) X1,X2,UD
    81 FORMAT(6X,'13MNP1 AT T1,M1,3X,M1=,3E17.8)
    B1 = GAM*RR1
    82 = -B1*RR1-MM(NPT)*CP(NPT)/(R*TT1)
    X1 = XX(Y)
    X2 = YY(Z)
    83 = UD*(AA*X1+BB*X2+1.)
    X2 = X2-1.
170 IF(IDERUG) WRITE(6,84) X1,X2,UD
    84 FORMAT(6X,'16MNP1 AT P1,M1,M1,3X,M1=3E17.8)
    B1 = 0.
    85 = -MM(NPT)/(R*TT1)
    X1 = XX(Y)+1000.
    X2 = YY(Z)+1000.
    OUD = UD*(AA*X1+BB*X2)
180 IF(IDERUG) WRITE(6,85) X1,X2,UD
    85 FORMAT(6X,'20HH1 AT T1,P1,M1 =3E17.8)
    C
185 150 K = 0
    IF(17P.EQ.NPT.ND.IF-K-2.NT-OR.TT.EQ.0.) GO TO 860
    K = NPT
    IF(NPT.NE.13) GO TO 870
    C
    C OUTPUT
    C
190 860 WRITE(6,5)
    5 FORMAT(1H1,42X,'46HDETUNATION PROPERTIES OF AN IDEAL REACTING GAS ')
    CALL OUT1
    WRITE(6,46)
195 46 FORMAT(13H UNBURNED GAS//)
    FMT(4)=FMT13
    FMT(5)=F8
    FMT(7)=F4
    WRITE(6,FMT)FP1,FP(2),FB,FB,(PUB(J),J=1,NPT)
    FMT(7)=F2
    WRITE(6,FMT)FT1,FT(2),FB,FB,(TUB(J),J=1,NPT)
    WRITE(6,FMT)FM1,FM(2),FB,FB,(H1(J),J=1,NPT)
    80-56 I=.NPT
    V(I)=AM1
    SONVEL(I) = (RR*GM1(I)*TUB(I)/AM1)**.5
205 56 CONTINUE
    FMT(7)=F3
    WRITE(6,FMT) FN1,F1(2),FM(3),FB,(V(J),J=1,NPT)
    FMT(7)=F4
    WRITE(6,FMT)FCP1,FC(2),FC(3),FC(4),(CP(J),J=1,NPT)
    WRITE(6,FMT)FG(1),FG1,FB,FB,(GM1(J),J=1,NPT)
    FMT(7)=F1
    WRITE(6,FMT){FL(I),I=1,4},{SONVEL(J),J=1,NPT}
```



```

215      WRITE(6,55)
55      FORMAT(11HBOURNED GAS//)
      FMT(4)=FMT(6)
      CALL OUT2
      WRITE(6,56)
68      FORMAT(22HDETENTIONATION PARAMETERS //)
      FMT(7)=F4
220      DO 70 I=1,NPT
          V(I)=PPF(I)/PUB(I)
          PCP(I)=IT(I)/TUB(I)
          SONVEL(I)=SONVEL(I)*RRHO(I)
70      CONTINUE
225      WRITE(6,FMT)FPP,FB,FB,FB,IV(I),J=1,NPT)
      WRITE(6,FMT)FIT,FB,FB,FB,PCP(J),J=1,NPT)
      DO 73 I=1,NPT
          V(I)=MM(I)/AM1
73      CONTINUE
      FMT(7)=F4
230      WRITE(6,FMT)FPM,FB,FB,FB,IV(I),J=1,NPT)
      WRITE(6,FMT)FRA,FR3,FB,FB,RRHO(J),J=1,NPT)
      WRITE(6,FMT)FMA,FMB,FB,FB,VMOC(J),J=1,NPT)
      FMT(7)=F1
235      WRITE(6,FMT) FUD,FL(2),FL(3),FL(4),(SONVEL(J),J=1,NPT)
          EQL=.TRUE.
      CALL OUT3
240      865 IF(K.EQ.0) GO TO 1000
          WRITE(6,865)
          868 FORMAT(1M1)
          NPT = 0
          870 NPT = NPT + 1
          C
          C      SAVE COMPOSITIONS FOR ESTIMATES OF NEXT POINT
          C
245      DO 880 I = 1,NS
          EN(I,NPT) = EN(I,K)
          880 CONTINUE
          902 CONTINUE
250      1000 TP = .FALSE.
          RETURN
          ENC

```

1712 00613  
1712 00614  
1712 00615  
1712 00616  
1712 00617  
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1712 00638  
1712 00639  
1712 00640  
1712 00641  
1712 00642  
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1712 00646  
1712 00647  
1712 00648  
1712 00649  
1712 00650  
1712 00651  
1712 00652





	C	SINGULAR MATRIX	P1712	00759
110	C	774 IF(.NOT.CONVG) GO TO 775 WRITE(6,172) 172 FORMAT(24HDERIVATIVE MATRIX SINGULAR ) IC = .TRUE.	P1712	00760
115		GO TO 171 775 IF (.NOT.HP.OR.NPT.NE.1.OR.NC.EQ.0.UR.IT.GT.108.) GO TO 371 WRITE(6,174)	P1712	00761
120		74 FORMAT(16HOSINGULAR MATRIX) IF(IC) GO TO 973 IF (.ISING) GO TO 937 NIZERO = 0 GO TO 873	P1712	00762
125		965 DC-970 JJ = 1, NS IF(IUSE(JJ)) 97C,968,967 967 IF(EN(JJ,NPT).EQ.0.) GO TO 873 GO TO 969	P1712	00763
130		96A EN(JJ,NPT) = NE.U.) GO TO 969 EN(JJ,NPT) = SMALNC ENTNUJJ - SMOL GO TO 970	P1712	00764
135		96Q NIZERO = NIZERO+1 970 CONTINUE IF(.NOT.IC) GO TO 971 IC = .FALSE. GO TO 83	P1712	00765
140		971 ISING = .TRUE. WRITE (6,776) 775 FORMAT (4HDRESTART) GO TO 43	P1712	00766
145		997 IF(NIZERO.NE.(L-1)) GO TO 873 IF(ENRAT,GT.1.00001.DK+ENRAT,LT.0.99999)-GO TO-873 ENN=0. NN=0 DO 83 I=1,L JEN=0 DO 80 J=1,NS IF(EN(J,NPT),EQ.0.) GO TO-88 IF(A(I,J).EQ.0.) GO TO 83 IF(JEN.NE.0) GO TO 83 JEN = J 80 CONTINUE NEA = NEN+1 EN(JEN,NPT) = 8C(I+Y,I,J)EN	P1712	00767
150		83 CONTINUE IF(NEN.LT.NIZERO) GO TO 373 CONVG = .TRUE. IC = .TRUE.	P1712	00768
155			P1712	00769
			P1712	00770
			P1712	00771
			P1712	00772
			P1712	00773
			P1712	00774
			P1712	00775
			P1712	00776
			P1712	00777
			P1712	00778
			P1712	00779
			P1712	00780
			P1712	00781
			P1712	00782
			P1712	00783
			P1712	00784
			P1712	00785
			P1712	00786
			P1712	00787
			P1712	00788
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			P1712	00790
			P1712	00791
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			P1712	00800
			P1712	00801
			P1712	00802
			P1712	00803
			P1712	00804
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			P1712	00806
			P1712	00807
			P1712	00808
			P1712	00809
			P1712	00810
			P1712	00811



215	IF (IUSE(J).EQ.0) FNEG2=FNEG2-ENLN(J)*TH WRITE (6,325) SUB(J,1),SUB(J,2), 1SUB(J,3),EN(J,NPT),ENLN(J),DELN(J),H3(J),S(J),FNEG1,FNEG2 925 FORMAT (1X,3A4,7E15.5) 926 CONTINUE WRITE (6,110) 110 FORMAT (1H0)	P1712 00865 P1712 00866 P1712 00867 P1712 00868 P1712 00869 P1712 00870 P1712 00871 P1712 00872 P1712 00873 P1712 00874 P1712 00875 P1712 00876 P1712 00877 P1712 00878 P1712 00879 P1712 00880 P1712 00881 P1712 00882 P1712 00883 P1712 00884 P1712 00885 P1712 00886 P1712 00887 P1712 00888 P1712 00889 P1712 00890 P1712 00891 P1712 00892 P1712 00893 P1712 00894 P1712 00895 P1712 00896 P1712 00897 P1712 00898 P1712 00900 P1712 00901 P1712 00902 P1712 00903 P1712 00904 P1712 00905 P1712 00906 P1712 00907 P1712 00908 P1712 00909 P1712 00910 P1712 00911 P1712 00912 P1712 00913 P1712 00914 P1712 00915 P1712 00916 P1712 00917
220	C C C 111 SUM = 0. DO 113 J=1,NS 112 ENLN(J)=ENLN(J)+AMBDA*DELN(J) EN(J,NPT) = 0. IF (ENLN(J)-ENLN+SIZE).LE.0.) GO TO 113 EN(J,NPT) = EXP(ENLN(J)) SUM = SUM+EN(J,NPT) GO TO 113	
225	114 EN(J,NPT) = EN(J,NPT) + AMBDA * DELN(J) 115 CONTINUE SUMN = SUM IF (TP) GO TO 115 TLN= TLN+AMBDA*DLNT TL= EXP(TLN) 115 ENLN = ENLN+AMBDA*X(IG1) ENN = EXP(ENLN) IF (LLHT(L).NE.1E) GO TO 116	
235	C C C CHECK ON REMOVING IONS DO 1116 J = 1,NS IF (A(L,J).EQ.0.) GO TO 1116 IF (EN(J,NPT).GT.0.) GO TO 116 1116 CONTINUE DO 1118 J=1,NS IF (A(L,J).NE.0.) IUSE(J) = -10000 1118 CONTINUE L = L-1 IG1 = IG1-1 GO TO 43	
245	C C C TEST FOR CONVERGENCE 116 IF (ITNU*8.EQ.0) GO TO 13 IF (AMBDA.LT.1.) GO TO 43 SUM = (ENN-SUMN)/ENN IF (SUM.LT.0.) SUM = -SUM IF (SUM.GT.0.5E-5) GO TO 43 DO 130 J=1,NS IF (IUSE(J).LT.0) GO TO 139 AA= DELN(J)/SUMN IF (AA.LT.0.) AA=-AA	
255		
260		
265		

```

IF (IUSE(J).EQ.0) NE=AREN(J,NPT)
129 IF (AA.GT.0.5E-5) GO TO 43
130 CONTINUE
13 CONVG= .TRUE.
270 IF (TT.LT.1LO+.OR.IT.GT.1HIGH+.AND.10E3UG) WRITE(6,336) IT,NPT
306 FORMAT(17H) THE TEMPERATURE=12.4,26H IS OUT OF RANGE FOR PCINT,15)
IF (IT.NE.0) GO TO 167
WRITE(6,973) IT,NPT
973 FORMAT(17H) 12,59H ITERATIONS DID NOT SATISFY CONVERGENCE REQUIRE
METS FOR THE POINT 15)
IF (.NOT.HP.OR.APV.NE.1.OR.NC.EQ.0.OR.IT.GT.100.) GO TO 873
WRITE(6,874)
IT=IT+1
RETURN
C
280 C CONVERGENCE TESTS ARE SATISFIED, TEST CONDENSED SPECIES.
C
C
160 IF (NC.EC.0) GO TO 143
SIZE=0
INC=0
DO 170 J=1,NS
IF (IUSE(J).EQ.0 .OR. IUSE(J).EQ.-10000) GO TO 170
INC=INC+1
IF (IDERUG) WRITE(6,144)(SU3(J,I),I=1,3),TEMP(INC),TEMP(INC+2),
IUSE(J),TEMP(INC,NPT)
144 FORMAT (1H) 3A4,2F10.3,3X,5HUSE=,14,215.7)
IF (TEMP(INC,NPT)) 146,146,159
146 IF (J.NE.JSOL .AND. J.NE.JLIQ) GO TO 147
JSOL=0
JLIQ=0
147 IF (J.EQ.1) GO TO 153
EN(J,NPT)=0.
GO TO 166
148 KC=1
IF (IUSE(J).EQ.-1) IUSE(J+1) GO TO 154
IF (J.EQ.1.OR.IUSE(J).NE.-IUSE(J-1)) GO TO 153
KC=1
154 JAG=J+KC
IF (CENTXG(NPT).LT.0.) GO TO 170
TKELT=TEMP(INC,1)
TMP=INC+KC
IF (TKELT.EQ.TEMP(IMP,2)) GO TO 154
TKELT=TEMP(IMP,2)
IF (TKELT.EQ.TEMP(IMP,1)) GO TO 157
WRITE(6,156)
156 FORMAT (50H) 3 PHASES OF A CONDENSED SPECIES ARE OUT OF ORDER )
C
C JTM SPECIES A SOLID (EN=0), (J+KC)TH SPECIES A LIQUID (EN IS +)
C
157 IF (TT.GT.TMELT) GO TO 169
IF (P.AND.IT.EQ.TMELT) GO TO 165
IF (TP) GO TO 1165
IF (TT.LE.TMELT-150.) GO TO 1165

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```

320      JSQ = J
      JLIQ = JKG
      GO TO 159

      C
      C JTH SPECIES A LIQUID(EN=0), (J*KG)TH SPECIES A SOLID (EN IS +)
      C
325      IF (TT.LT.TMELT) GO TO 169
      IF (TP.AND.TT.EQ.TMELT) GO TO 169
      IF (TP) GO TO 1165
      IF (TT.GE.TMELT+150.) GO TO 1165
      JSOL = JKG
      JLIQ = J
330      TTN = ATG(TMELT)
      TT = TMELT
      EN(JKG,NPT) = .5 * EN(JKG,NPT)
      EN(J,NPT) = EN(JKG,NPT)
      GO TO 165

335      C
      C WRONG PHASE INCLUDED FOR T INTERVAL, SWITCH EN
      C
340      1165 EN(J,NPT) = EN (JKG, NPT)
      IUSE(J) = -IUSE(J)
      IUSE (JKG) = -IUSE(JKG)
      EN(JKG,NPT) = 0.
      GO TO 160

345      153 IF (TT.LT.TEMP(INC,1) .AND. TEMP(INC,1).NE.110N) GO TO 169
      IF (TT.GT.TEMP(INC,2)) GO TO 169

      C
      C
      SUM = 0.
      DO 167 I = 1, L
      SUM = SUM + A(I,J)*X(I)
350      167 CONTINUE
      DELF = H(J)-S(J)-SUM
      IF (IDEBUG) WRITE(6,168)DELF,SIZEF
      168 FORMAT (17H GO-SUM(AIJ*PI) =E15.7,10X,18HPREVIOUS DELTA S =,E15.7)
      IF (DELF.GE.SIZEF) FORK = DELF.GE.0. GO TO 169
      SIZEF = DELF
      JOELF = J
355      169 IF (INC.EQ.NC) GO TO 1160
      170 CONTINUE
      1160 IF (SIZEF.EQ.0.) GO TO 143
      J = JOELF

360      165 IC1 = IC1 + 1
      166 IUSE(J) = - IUSE(J)
      166 CONVG = .FALSE.
      163 TN = NUM9
      IF (IDEBUG) WRITE(6,771) NPT, (X(IIL),IL=1,L), TN
      771 FORMAT (13,14F9.3)
      ITNUM9 = ITN
      GO TO 143

370      C
      C CALCULATE EQUILIBRIUM PROPERTIES

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P1712 00971  
P1712 00972  
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P1712 01016  
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P1712 01018  
P1712 01019  
P1712 01020  
P1712 01021  
P1712 01022  
P1712 01023



SUBROUTINE	EQ-ARM	FORTRAN EXTENDED VERSION 2.0	31/12/70	06.05.56.	PAGE NO. 8
171	SSUM(NPT) = 0.			P1712	01024
	IF(JLID,NE,0) EN(JSOL,NPT)=ENSOL			P1712	01025
375	DO 183 J=1,NS			P1712	01026
	IF (NPT,EQ,1) SS0 = SS0 + EN(J,1)*S(J)			P1712	01027
	SS = S(J)			P1712	01028
	IF(IUSEVOT,EQ,0) SS=SS-EN(N(J),1)			P1712	01029
	SSUM(NPT) = SSUM(NPT)+SS*EN(J,NPT)			P1712	01030
380	CONTINUE			P1712	01031
	IF(.NOT.IC) GO TO 176			P1712	01032
	GLVPT(NPT) = -1.			P1712	01033
	OLVPT(NPT) = 1.			P1712	01034
	CPR(NPT) = CPSUM			P1712	01035
385	GO TO 199			P1712	01036
	SUM = 0.			P1712	01037
178	DO 179 J = 1,L			P1712	01038
	SUM = SUM + PROK(J)*X(J)			P1712	01039
179	CONTINUE			P1712	01040
390	OLVPT(NPT) = -2.*SUM/ENN*X(IQ1)			P1712	01041
	IF(JLIC,EQ,0) GO TO 199			P1712	01042
	IUSE(JLIC) = -IUSE(JLIC)			P1712	01043
	HSUM(NPT) = HSUM(NPT)+EN(JLIC,NPT)*(H0(JLIC)-H0(JSOL))			P1712	01044
	IQ1 = IQ1+1			P1712	01045
395	GAMMAS(NPT) = -1./OLVPT(NPT)			P1712	01046
	GO TO 185			P1712	01047
5	199 GAMMAS(NPT) = -1./ (OLVPT(NPT) + (OLVPT(NPT)**2)*ENN/CPR(NPT))			P1712	01048
	ITT(NPT) = TT			P1712	01049
400	PP(NPT) = PP			P1712	01050
	CPR(NPT) = CPSUM			P1712	01051
	HSUM(NPT) = HSUM(NPT)+TT			P1712	01052
	ITT(NPT) = 1./ENN			P1712	01053
405	200 IF (.NOT.IDEBUG) RETURN			P1712	01054
	WRITE(6,201) NPT,PCPINPT),PP,ITT,HSUM(NPT),SSUM(NPT),WM(NPT),CPR(NPT)			P1712	01055
	17).OLVPT(NPT),OLVPT(NPT),GAMMAS(NPT)			P1712	01056
	201 FORMAT (7HOPINT=I3,X,4HPCP=E13.6,X,2HP=E13.6,X,2HT=E13.6,X,4H			P1712	01057
	1H/R=E13.6,X,4HHS/R=E13.6/X,3HMM=E13.6,X,5HCP/R=E13.6,X,6HDI,VPT			P1712	01058
	2=E13.6,X,6HOLVPT=E13.6,X,9MGAMMA(S)=E13.6 )			P1712	01059
	GO TO 1000			P1712	01060
410	C			P1712	01061
	C			P1712	01062
	C			P1712	01063
873	TT=0.			P1712	01064
873	ITT=0.			P1712	01065
415	1000 RETURN			P1712	01066
	END			P1712	01067
				P1712	01068

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## SUBROUTINE FROZEN

C

C

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05

{FROZEN COMPOSITION EXPANSION ONLY}

LOGICAL EQL,FROZ,CONVG

10

```
COMMON/POINTS/RSUM(13),SSUN(13),CPR(13),OLVTP(13),OLVPT(13)
1  GAMMAS(13),PIZ(26),Y(26),V(13),PPF(13),WM(13),SONVEL(13),YTT(13)
2  TCTN(13)
COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)
1  DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)
```

15

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COMMON/RTSC/ENN,SUMN,TT,SH,ATGR(13,101),LLRT(15),BU(15,2)
1  TM,TLCH,TMIO,THIGH,PF,SH,UN,OF,EORAT,FPCT,R,RR,HSUB90,AC(2),AM(2)
2  HPP(2),RHO(2),VMIN(2),LS(2),MP(2),DATA(22),NAME(15,5)
3  ANUM(15,5),PECHT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)
4  RHOP,RHM(15),TLN,JANF
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20

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COMMON/INDX/ IOEBUG,CONVG,IP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,L,NS,
1  KHAT,INAT,TOL,N,J,NOMIT,IP,NEWK,NSUB,NSUP,ITR,GPCVFR,CPCEVO
2  IONS,AC,NSERT,JSOL,JLIO,KASE(14),NREAC,IC,IQ2
COMMON/PERF/PCP(26),VMOC(13),SPIN(13),VACI(13),SUBAR(13),SUPAR(13)
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```
1  CPRF(13),AEAT(13),CSTR,EQL,FROZ,SSO
COMMON/OUP/FT(30),FP(4),FT(4),FH(4),FS(4),FM(4),FV(4),FD(4)
1  FG(4),FG(4),FB,FHT13,F1,F2,F3,F4,F5,FL(4),FMT19,FA1,FA2
2  FRI,FCI,FN(4),F(4),FA(4),FI(4),FMT9X,F0
```

30

```
ITROT = 3
EQL = .FALSE.
NPT = 2
TT = TTT(1)
TLN=ALOG(TT)
```

35

```
GAMMAS(I) = CPRF(I)/CPRF(I)*1.7*W(1)
CPR(1) = CPRF(1)
PCP(2) = ((GAMMAS(1)+1.)/2.)*((GAMMAS(1)/(GAMMAS(1)-1.))
DATA(1) = 2./(GAMMAS(1) + 1.)
TLN = TLN + ALOG(DATA(1))
DO 902 IP=2,NP
```

40

```
IF(NPT.EQ.2) GO TO 45
PCP(NPT) = P(1)/P(IP)
CONVG = .FALSE.
PCPLH=ALOG(PCP(NPT))
S0 = SSO -PCPLN/NM(1)
SUMH = 0.
```

45

```
51 TT=EXP(TENT)
SUNS=0.
J = 1
NNA = NPT
NPT = 1
CALL GPHS
NPT = NM
```

50

```
DO 60 J=1,NS
IF(EN(J,1).EQ.0.) GO TO 63
SUMS = SUMS + S(J)*EN(J,1)
IF(CONVG) SUMH=SUMH+H0(J)*EN(J,1)
```

55	60 CONTINUE	P1712 01122
	IF (CONVG) GO TO 81	P1712 01123
	ULNT=(SUMS-50)/CPSUM	P1712 01124
	TUA=TLN-ULNT	P1712 01125
	IF (DLNT.LT.0.) DLNT=-DLNT	P1712 01126
	IF (DLNT.LT.0.5E-4) CONVG=.TRUE.	P1712 01127
60	GO TO 51	P1712 01128
	81 ITI(NPT)= IT	P1712 01129
	SSUM(NPT)= SSUM(1)	P1712 01130
	HSUM(NPT)= IT*SUM	P1712 01131
	GAMMAS(NPT)= CPSUM/(CPSUM-1./NM(1))	P1712 01132
65	IF (IP.GT.2) GO TO 90	P1712 01133
	GO TO 51	P1712 01134
	C	P1712 01135
	C	P1712 01136
	C	P1712 01137
70	OH = HSUM(1)-HSUM(2)	P1712 01138
	OHSTAR = OH-(GAMMAS(2)*TT/(2.*NM(1)))	P1712 01139
	OH = OHSTAR/OH	P1712 01140
	IF (OH.LT.0.) OH=-OH	P1712 01141
	IF (OH.LT.0.4E-4.OR.ITROT.EQ.0) GO TO 90	P1712 01142
75	PCP(2) = PCP(2)/(1.+2.*OHSTAR*NM(1)/(IT*(GAMMAS(2)+1.)))	P1712 01143
	P(2) = P(1)/PCP(2)	P1712 01144
	ITROT = ITROT-1	P1712 01145
	GO TO 45	P1712 01146
	90 NPT(NPT)= NPT(1)	P1712 01147
	PP(NPT) = P(IP)	P1712 01148
80	CPR(NPT)= CPSUM	P1712 01149
	K = 0	P1712 01150
	IF (TT.LT.(TLOW-150.)) GO TO 903	P1712 01151
	IF (NC.EQ.0) GO TO 700	P1712 01152
	INC = 1	P1712 01153
85	DO 901 I=1,N5	P1712 01154
	IF (IUSE(I).EQ.0.OR.IUSE(I).EQ.-10000) GO TO 901	P1712 01155
	INC = INC+1	P1712 01156
	IF (EM(I).EQ.0.) GO TO 901	P1712 01157
	IF (TT.LT.(TEMP(INC)-50.)) OR (TT.GT.(TEMP(1)+50.)) GO TO 903	P1712 01158
90	901 CONTINUE	P1712 01159
	700 IF (IP.EQ.NP) GO TO 863	P1712 01160
	K = NPT	P1712 01161
	IF (NPT.NE.13) GO TO 870	P1712 01162
	GO TO 863	P1712 01163
95	903 NPT = NPT - 1	P1712 01164
	863 GALT=RTROT	P1712 01165
	IF (NSUB+NSUP.NE.0) CALL RATIO	P1712 01166
	865 IF (K.EQ.0) GO TO 1002	P1712 01167
	NPT = 2	P1712 01168
100	870 NPT = NPT + 1	P1712 01169
	902 CONTINUE	P1712 01170
	1000 RETURN	P1712 01171
	END	

	C	SUBROUTINE HCALC	P1712 01172
	C	CALCULATE ENTHALPY FOR PROPELLANT USING COEFFICIENTS	P1712 01173
05	C	LOGICAL MOLES	P1712 01174
		DIMENSION NUM(15),S(2)	P1712 01175
			P1712 01176
			P1712 01177
	C	COMMON/SPACES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),M0(150)	P1712 01178
		1,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)	P1712 01179
10		COMMON/MISC/ENR,SUMN,IT,S0,ATOM(1,10),LLMT(15),30(15),80P(15,2)	P1712 01180
		1,FM,7LCM,THIO,THIGH,PP,CPSUM,OF,EGRAT,FPST,R,RR,MSUB0,AC(2),AM(2)	P1712 01181
		2,HP(12),RHO(12),VMIN(2),VPLS(12),MP(2),DATA(22),NAME(15,5)	P1712 01182
		3,ANUM(15,5),PECHT(15),ENTH(15),FAZ(15),RTMP(15),FOX(15),DENS(15)	P1712 01183
15		4,RHOP,RHM(15),TLN,JANF	P1712 01184
		COMMON/INCH/ IDEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,L,NS,	P1712 01185
		1,KHAT,IMAT,IQI,N,J,NOMIT,IP,NEWQ,NSUB,NSUP,IIN,CPCVFR,CPCVED	P1712 01186
		2,IONS,NC,INSERT,JSOL,JLIQ,KASE(14),NREAC,IC,IQ2	P1712 01187
20		EQUIVALENCE(ANUM,NUM)	P1712 01188
			P1712 01189
	C	DATA AG/1HG/,IZERO/2H00/,OX/1H0/	P1712 01190
25	C	IS IT IN RANGE	P1712 01191
		IF(IT.LI.(TLOW-100.).OR.IT.GT.(THIGH+1000.))GO TO 80	P1712 01192
		NS(1) = 0.	P1712 01193
		NS(2) = 0.	P1712 01194
		HP(1) = 0.	P1712 01195
30		HP(2) = 0.	P1712 01196
		AC(1) = 0.	P1712 01197
		AC(2) = 0.	P1712 01198
		DO 900 N=1,NREAC	P1712 01199
		K=2	P1712 01200
35		IF(FOX(N).EQ.OX)K=1	P1712 01201
		PCNT=PECHT(N)	P1712 01202
		IF(THOLES)PCNT=PCNT+RHM(N)	P1712 01203
		WS(K) = WS(K) + PCNT	P1712 01204
		J = NUM(N,5)	P1712 01205
40		IF (J.NE.3) GO TO 90	P1712 01206
		DO 11 J=1,L	P1712 01207
		DATA(J)=0.	P1712 01208
		10 CONTINUE	P1712 01209
		DO 40 I=1,4	P1712 01210
45		IF(ANUM(N,I).EQ.0.)GO TO 50	P1712 01211
		DO 20 J=1,L	P1712 01212
		IF(ILLMT(J).EQ.NAME(N,I)) GO TO 30	P1712 01213
		20 CONTINUE	P1712 01214
		30 DATA(J)=ANUM(N,I)	P1712 01215
50		40 CONTINUE	P1712 01216
		50 IS=0	P1712 01217
		DO 70 J=1,NS	P1712 01218
		IF(IUSE(J).EQ.0)GO TO 55	P1712 01219
			P1712 01220
			P1712 01221
			P1712 01222
			P1712 01223
			P1712 01224

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55      IS = IS+1
      IF (FAZ(N).EQ.AG) GO TO 70
      IF (IT.LY.TEMP(IS,1).OR.IT.JT.TEMP(IS,2)) GO TO 70
      GO TO 56
56      IF (FAZ(N).EQ.AG) GO TO 70
56      DO 60 I=1,L
      IF (AT, JT, NE, DATA(I)) GO TO 70
      60 CONTINUE
      NUM(N,5) = J
      GO TO 90
      70 CONTINUE
      GO TO 80
56      NSS = NS
      NS = J
      CALL CP+S
      GPSUM = GPSUM/EN(J,HPT)
      NS = NSS
      IF (H0(J).GT.-.01 .AND. H0(J).LT..01) H0(J) = 0.
      RTEMP(N) = IT
      ENTH(N) = HU(J)*RT
      AC(N) = AC(K)+GPSUM*PCHT/RMW(N)
      HPP(K) = HPP(K)+ENTH(N)*PCWT/RMW(N)
      500 CONTINUE
      DO 950 K=1,2
      IF (HPT(K).EQ.0) GO TO 950
      HPP(K) = HPP(K)/WS(K)
      AC(K) = AC(K)/WS(K)
      950 CONTINUE
      HSUB9 = (HP(1)*HPP(1)+HP(2)*HPP(2))/(HP(1)+HP(2))
      GO TO 1000
      80 WRITE(95) N
      85 FORMAT(1H0,12,34HITH REACTANT IS NOT IN THERMO DATA )
      1300 RETURN
      END

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P1712 01225  
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 P1712 01257  
 P1712 01258

		P1712	U1259
	SUBROUTINE MATRIX	P1712	U1259
	DOUBLE PRECISION G,X	P1712	U1260
	LOGICAL HP,SP,IF,IOEBUG,CONVG,NEWK	P1712	U1261
05		P1712	U1262
		P1712	U1263
		P1712	U1264
	COMMON/POINTS/HSUB(13),SSUM(13),CPR(13),DLVTP(13),ULVPT(13)	P1712	U1265
	1, GANVAS(13),P(26),T(26),V(13),PPP(13),WM(13),SONVEL(13),TTT(13)	P1712	U1266
	2,TCIN(13)	P1712	U1267
10	COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),ENLN(150),M0(150)	P1712	U1268
	1, DELN(15),A(15,150),SUB(15,3),IUSE(150),TEMP(50,2)	P1712	U1269
	COMMON/MISC/ENN,SUMN,TT,SU,ATON(3,14),LLMT(15),BO(15),BOP(15,2)	P1712	U1270
	1,TR,TLCK,TNID,THIGH,PF,CPSUM,OF,EORAT,FPCT,R,PR,HSUB0,ACT2),AM(2)	P1712	U1271
	2,PPP(2),RMO(2),VMIN(2),VPLS(2),MP(2),DATA(22),NAME(15,5)	P1712	U1272
15	3, ANUM(15,7),PECHT(15),ENTH(15),FAZ(15),RIEMP(15),FOX(15),DENS(15)	P1712	U1273
	4, RHOP, RMH(15),TLN,JANF	P1712	U1274
	COMMON /DOUBLE/ G(20,21), X(20)	P1712	U1275
	COMMON/INDEX/ IOEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,L,NS,	P1712	U1276
	1,KNAT,IMAT,IOI,N:J,NOMIT,IP,NEWK,NSUB,NSUP,ITN,CPCVFR,CPCVED	P1712	U1277
20	2,IONS,AC,NSERT,JSOL,JLJO,KASE(14),NREAC,IO,IO2	P1712	U1278
	IO2 = IO1 + 1	P1712	U1279
	IO3 = IO2 + 1	P1712	U1280
	KNAT = IO3	P1712	U1281
	IF(.NOT.CONVG.AND.TP) KNAT = IO2	P1712	U1282
	IMAT = KNAT - 1	P1712	U1283
25		P1712	U1284
	CLEAR MATRIX STORAGES TO ZERO	P1712	U1285
30	DO 211 I=1,IMAT	P1712	U1286
	DO 211 K=1,KNAT	P1712	U1287
	G(I,K) = 0.000	P1712	U1288
	G(I,K) = 0.0	P1712	U1289
35	211 CONTINUE	P1712	U1290
	SSS = 0.	P1712	U1291
	HSUM(NPT) = 0.	P1712	U1292
		P1712	U1293
	BEGIN SET UP OF ITERATION MATRIX	P1712	U1294
40	KK = L	P1712	U1295
	DO 65 J=1,NS	P1712	U1296
	HSUB(J)*EN(J,NPT)	P1712	U1297
	IF (IUSE(J)) 65,11,70	P1712	U1298
45	1) F = (H0(J)-S(J)+ENLN(J)+IN)*EN(J,NPT)	P1712	U1299
	SS = M-F	P1712	U1300
	TERM1 = H	P1712	U1301
	IF (KNAT.EQ. IO2) TERM1 = F	P1712	U1302
	DO 55 I = 1, L	P1712	U1303
50	CALCULATE THE ELEMENTS R(I,K)	P1712	U1304
	IF (A(I,J).EQ. 0.) GO TO 55	P1712	U1305
	TERM= A(I,J)*EN(J,NPT)	P1712	U1306
		P1712	U1307
		P1712	U1308
		P1712	U1309
		P1712	U1310
		P1712	U1311

55	DC 15 K=1, C	P1712 01312
	G(I,K) = G(I,K) + A(I,J)*TERM	P1712 01313
	15 CONTINUE	P1712 01314
	C	P1712 01315
60	G(I,IQ1)=G(I,IQ1)+TERM	P1712 01316
	G(I,IQ2)=G(I,IQ2)+A(I,J)*TERM1	P1712 01317
	IF (CONVG=.OR. F) GO TO 55	P1712 01318
	G(I,IQ3) = G(I,IQ3)+A(I,J)*F	P1712 01319
	IF (SP) G(IQ2,I) = G(IQ2,I) + A(I,J)*SS	P1712 01320
	55 CONTINUE	P1712 01321
65	IF (KNAT .EQ. IC2) GO TO 64	P1712 01322
	IF (CONVG.OR.HP) GO TO 59	P1712 01323
	G(IQ2,IQ1) = G(IQ2,IQ1) + SS	P1712 01324
	G(IQ2,IQ2)=G(IQ2,IQ2)+H0(J)*SS	P1712 01325
	G(IQ2,IQ3) = G(IQ2,IQ3)+(S(J) - EMLN(J)-TM)*F	P1712 01326
	GO TO 62	P1712 01327
70	59 G(IQ2,IQ2)=G(IQ2,IQ2)+H0(J)*H	P1712 01328
	IF (CONVG) GO TO 64	P1712 01329
	G(IQ2,IQ3)=G(IQ2,IQ3)+H0(J)*F	P1712 01330
	62 G(IQ1,IQ3)=G(IQ1,IQ3)+F	P1712 01331
	64 G(IQ1,IQ2)=G(IQ1,IQ2)+TERM	P1712 01332
	GO TO 65	P1712 01333
75	C	P1712 01334
	C CONDENSED SPECIES	P1712 01335
	70 KK = KK + 1	P1712 01336
80	00 75 I = 1, L	P1712 01337
	G(I,KK) = A(I,J)	P1712 01338
2	G(I,KK) = G(I,KK) - A(I,J)*EN(J,NPT)	P1712 01339
	75 CONTINUE	P1712 01340
	G(KK,IQ2) = H0(J)	P1712 01341
85	G(KK,KK) = H0(J) - S(J)	P1712 01342
	MSUM(NPT) = MSUM(NPT) + M	P1712 01343
	IF (.NOT.SP) GO TO 55	P1712 01344
	SSS = SSS + S(J)*EN(J,NPT)	P1712 01345
	G(IQ2,KK) = S(J)	P1712 01346
90	65 CONTINUE	P1712 01347
	SSS = SSS + G(IQ2,IQ1)	P1712 01348
	MSUM(NPT) = MSUM(NPT) + G(IQ1,IQ2)	P1712 01349
	G(IQ1,IQ1) = SUM - ENN	P1712 01350
95	C	P1712 01351
	C REFLECT SYMMETRIC PORTIONS OF THE MATRIX	P1712 01352
	ISYM = IQ1	P1712 01353
	IF (HP.OR.CONVG) ISYM=IQ2	P1712 01354
100	00 102 I=1, ISYM	P1712 01355
	00 102 J=I, ISYM	P1712 01356
	G(J,I)=G(I,J)	P1712 01357
	102 CONTINUE	P1712 01358
	C	P1712 01359
	C COMPLETE THE RIGHT HAND SIDE	P1712 01360
105	C	P1712 01361
	C IF (CONVG) GO TO 175	P1712 01362
		P1712 01363
		P1712 01364

```

110      DC 165 I=1,L
          X(I)=30(I)-G(I,IQ1)
          G(I,KMAT) = G(I,KMAT)+X(I)
          145 CONTINUE
          G(IQ1,KMAT) = G(IQ1,KMAT)+ENN-SUMN
          C
          C COMPLETE ENERGY ROW AND TEMPERATURE COLUMN
          C
          IF (KMAT.EQ. IC2) GO TO 105
          IF (SP)ENERGY = S0+ENN-SUMN - SSS
          IF (HP)ENERGY=HSUR0/TT - HSUM(NPT)
          G(IQ2,IC3)=G(IQ2,IC3)+ENERGY
          175 G(IQ2,IC2)=G(IC2,IC2)+CPSUM
          105 RETURN
          ENC
120

```

P1712 01365  
 P1712 01366  
 P1712 01367  
 P1712 01368  
 P1712 01369  
 P1712 01370  
 P1712 01371  
 P1712 01372  
 P1712 01373  
 P1712 01374  
 P1712 01375  
 P1712 01376  
 P1712 01377  
 P1712 01378  
 P1712 01379





```

55 28 IF (NN-I) 29,31,29
    29 DO 30 J=NN,IUSE1
        Z=G(I,J)
        G(I,J)=G(NN,J)
        G(NN,J)=Z
    30 CONTINUE

60 31 K = NN + 1
    32 DO 36 J = K, IUSE1
        IF (G(NN,NN) .EQ. 0.) GO TO 23
        G(NN,J) = G(NN,J) / G(NN,NN)
    36 CONTINUE
    IF (K-IUSE1) 86,45,38
    48 DO 44 I = K, IUSE1
        40 DO 44 J = K, IUSE1
            G(I,J) = G(I,J) - G(I,NN)*G(NN,J)
        44 CONTINUE
    45 CONTINUE

75 46 BACKSOLVE FOR THE VARIABLES
    47 K = IUSE1
    47 J = K + 1
    48 X(K) = 0.000
    49 X(K) = 0.3
    50 SUM = 0.0
    51 IF (IUSE1 - J) 51,45,48
    52 DO 50 I = J, IUSE1
        SUM = SUM + G(K,I) * X(I)
    50 CONTINUE
    51 X(K) = G(K,IUSE1) - SUM
    52 K = K - 1
    53 IF (K) 67,151,47
    67 RETURN
    151 END

```

P1712 01438  
 P1712 01439  
 P1712 01440  
 P1712 01441  
 P1712 01442  
 P1712 01443  
 P1712 01444  
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 P1712 01463  
 P1712 01464  
 P1712 01465  
 P1712 01466  
 P1712 01467  
 P1712 01468  
 P1712 01469  
 P1712 01470  
 P1712 01471

05	C	SUBROUTINE MOLIER	P1712 01472
		COMMON/POINTS/MSUM(13),SSUM(13),CPR(13),OLVFP(13),JLVFP(13)	P1712 01473
		1 ,GAMMAS(13),P(26),T(26),V(13),PPP(13),MM(13),SONVEL(13),TTT(13)	P1712 01474
		2 ,TCFN(13)	P1712 01475
		COMMON/SPECIES/DOEF(2,7,150),S(150),EN(150,13),EALN(150),MO(150)	P1712 01476
		1 ,TENT(150),A(15,150),SU(150,3),IUSE(150),TEMP(150,2)	P1712 01477
		COMMON/MISC/ERN,SUMM,II,SU,ATOM(13,10),LLM(15),BU(15),BDP(15,2)	P1712 01478
		1 ,TK,TLOM,THIO,THIGH,PP,CPSUM,OF,EGRAI,FPC,R,R,MSUBO,AC(2),AM(2)	P1712 01479
		2 ,MP(12),AMO(12),VMI(12),VPLS(12),MP(12),DATA(22),NAME(15,5)	P1712 01480
		3 ,ANUM(15,5),PCMF(15),ENT(15),FAZ(15),RTCMP(15),FOX(15),DEMS(15)	P1712 01481
		4 ,RHOP,R4M(15),ILN,JANF	P1712 01482
		COMMON/INDEX/IDCRUG,CONVG,IP,NP,SP,NDSF,TPSP,MOLES,NP,NT,L,NS,	P1712 01483
		1 ,KHA7,I7AT,I3I,N,J,NOMIT,IP,NEWZ,NSUB,ASUP,ITN,OPCVFR,CPCVED	P1712 01484
		2 ,IONS,NC,INSERT,J,SOL,JULIQ,KA5E(14),NREAC,IC,JO2	P1712 01485
		DO 91 IT = 1,26	P1712 01486
		IF (IT) EQ. 0.7 GO TO 95	P1712 01487
		NT = IT	P1712 01488
		91 CONTINUE	P1712 01489
20	C	SET ASSIGNED P	P1712 01490
	C	92 DO 902 IP = 1,NP	P1712 01491
		PP = P(IP)	P1712 01492
	C	SET ASSIGNED :	P1712 01493
25	C	DO 902 I3=1,NT	P1712 01494
	C	IT = (IT)	P1712 01495
		CALL EQLDRN	P1712 01496
30		IF (IT) EQ. 0.7 GO TO 302	P1712 01497
		IF (NP) EQ. 0.7 GO TO 1000	P1712 01498
		IF (IP) EQ. 0.7 GO TO 860	P1712 01499
35		K = 0	P1712 01500
		K = NPT	P1712 01501
		IF (NP) EQ. 0.7 GO TO 870	P1712 01502
		660 WRITE (6,5)	P1712 01503
		5 FORMAT(1H1,41X,6HTHERMODYNAMIC EQUILIBRIUM PROPERTIES AT ASSIGNED	P1712 01504
		1 ,/43X,28H TEMPERATURES AND PRESSURES ///	P1712 01505
40		CALL OUT1	P1712 01506
		WRITE (6,553)	P1712 01507
		963 FORMAT (25HTHERMODYNAMIC PROPERTIES//)	P1712 01508
		CALL OUT2	P1712 01509
		CALL OUT3	P1712 01510
45		IF (K) EQ. 0.7 GO TO 1000	P1712 01511
		WRITE (6,560)	P1712 01512
		560 FORMAT(1H1)	P1712 01513
		NPT = 0	P1712 01514
		970 NPT = NPT + 1	P1712 01515
50	C	SAVE COMPOSITIONS FOR ESTIMATES OF NEXT POINT	P1712 01516
	C	DO 880 I = 1,NS	P1712 01517
			P1712 01518
			P1712 01519
			P1712 01520
			P1712 01521
			P1712 01522
			P1712 01523
			P1712 01524

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55      EN(I,NFY) = EN(I,K)
      880 CONTINUE
      962 CONTINUE
      1000 RETURN
      END

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P1712 01525  
 P1712 01526  
 P1712 01527  
 P1712 01528  
 P1712 01529

SUBROUTINE OUT1		FORTRAN EXTENDED VERSION 2.0		SUBROUTINE OUT1	
C	C	DOUBLE PRECISION G,X		P1712	01530
C	C	LOGICAL EUL,FROZ ,TP,HP,SP,H2SP,T2SP,MOLES		P1712	01531
05	C	DIMENSION NV(13),Z(10,3),HEAD(15),YX(5),YM(5)		P1712	01532
	C			P1712	01533
	C			P1712	01534
	C			P1712	01535
	C			P1712	01536
10		COMMON/POINTS/MSUM(13),SSUM(13),CPR(13),OLVTP(13),OLVPT(13)		P1712	01537
		1 ,GAMMAS(13),P(26),T(26),V(13),PPP(13),MM(13),SCNVEL(13),FIT(13)		P1712	01538
		2 ,TOTN(13)		P1712	01539
		COMMON/SPECIES/CCEP(2,7,150),S(150),EN(150,13),ENLN(150),H0(150)		P1712	01540
		1 ,CELN(150),A(15,150),SUB(150,3),TUSE(150),TEMP(50,2)		P1712	01541
		COMMON/MISC/ENR,SUNN,T,T,SU,ATOM(3,101),LLMT(15),BT(15),BOP(15,2)		P1712	01542
		1 ,TM,T10M,T10D,THIGH,PP,CPSUM,OF,EQRAT,FCPT,N,RR,MSUBJ,AL(2),AM(2)		P1712	01543
15		2 ,MPP(2),RHO(2),VMIN(2),VPLS(2),NR(2),DATA(22),NAME(15,5)		P1712	01544
		3 ,ANUM(15,5),PECNT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)		P1712	01545
		4 ,RHCP,FMW(15),TLN,JANF		P1712	01546
		COMMON/DOUBLE/ G(20,21), X(20)		P1712	01547
		COMMON/INDEX/ IDEBUG,CORVG,TP,HP,SP,H2SP,T2SP,MOLES,NP,NT,NFI,L,NS,		P1712	01548
20		1 ,KMAT,IMAT,IOI,N,J,NHMT,IP,NEHR,NSUB,NSUP,ITN,QPCVFR,QPCVEQ		P1712	01549
		2 ,IONS,NC,NSERT,JSOL,JLIQ,KASE(14),NREAC,IC,IQ2		P1712	01550
		COMMON/PERF/PCP(26),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)		P1712	01551
		1 ,CPRF(13),AEAT(13),CSTR,EQL,FROZ,SSG		P1712	01552
		COMMON/OUT/FFMT(30),FPI(4),FI(4),FHI(4),FS(4),FV(4),FO(4)		P1712	01553
25		1 ,FCIT,FG(4),FB,FMT13,F1,F2,F3,F4,F5,F6,F7,F8,F9,F10,F11,F12,F13,F14,F15,F16,F17,F18,F19,F20		P1712	01554
		2 ,FRI,FCI,FN(4),FA(4),FA(4),FI(4),FNT9,FA1,FA2		P1712	01555
		COMMON/CVGLUM/ VOLUMC,IMPETUS,IFLGGG		P1712	01556
		COMMON/PERCENT/ PMULE		P1712	01557
30	C	REAL IMPETUS		P1712	01558
	C	EQUIVALENCE (V,NV1,Z,H0)		P1712	01559
	C	HEAD=(1H ,2A4.5 (A2,F8.5,3X)5 X,F7.5,F13.3,4X,A1,F10.2,F9.4)		P1712	01560
	C	DATA HEAD/4H(1H ,4H,2A4.2H,5.4H)2,4HF8.5 ,4H,3X)2H,5 .2HX,		P1712	01561
35		1 ,4HF7.5 ,4H,F13 ,4H,3.4 ,4HX,A1 ,4H,F10 ,4H,2.F ,4H9.4)/		P1712	01562
		DATA FUEL/7H(FUEL/7OXID/4H,OXID/ANT/3HANT/1OX/1MO/		P1712	01563
		1 ,YN/2H,1 ,2H,2 ,2H,3 ,2H,4 ,2H,5 /		P1712	01564
		2 ,YX/3H,57,3H,44,3H,31,3H,18,2H,5 /		P1712	01565
40	C	WRITE(6,4) KASE		P1712	01566
		4 FORMAT(1H0,13A6,A2)		P1712	01567
		5 FORMAT(9H CASE NO.,13)		P1712	01568
		IF(.NOT.MOLES) WRITE(6,5)		P1712	01569
45		5 FORMAT(77X,46HNT FRACTION ENTHALPY STATE TEMP DENSITY/		P1712	01570
		1 10X,16HCHEMICAL FORMULA,51X,21H(SEE NOTE: CAL/MOL,10X,5HDLG K,		P1712	01571
		2 4X,4HCVG/SEC )		P1712	01572
		IF(MOLES) WRITE(6,6)		P1712	01573
		6 FORMAT(10X,5HMOLES,2X,33HENTHALPY STATE---TEMP---DENSITY/		P1712	01574
50		1 10X,16HCHEMICAL FORMULA,67X,7HCVG/MOL,10X,13HDEG K		P1712	01575
		DO 15 N=1,NREAC		P1712	01576
		IF (FOX(N).EQ.FOX(N-1))GO TO 11		P1712	01577
		IF (FOX(N).NE.OX)GO TO 10		P1712	01578
				P1712	01579
				P1712	01580
				P1712	01581

```

55      HD1 = C*10
      HD2 = ANT
      GO TO 11
      10 HD1 = FUEL
      HD2 = FB
      11 DO 13 J=1,5
      13 CONTINUE
      14 J=J-1
      HD3(3)=YN(J)
      HD3(7)=YX(J)
      WRITE(6,HEAD)HD1,HD2,(NAME(N,JJ),ANUM(N,JJ),JJ,PECHT(N),ECHT
      1N),FAZ(N),RTMP(N),DENS(N)
      15 CONTINUE
      WRITE(6,20) OF,FCPT,EGRAT,RHOP
      20 FORMAT (1H0,15X, 4H0/F=, F8.4,4X,13HPERCENT FUEL=,F8.4,4X,
      1 19HEQUIVALENCE RATIO=,F7.4,4X,8HDENSITY=,F8.4//)
      C
      AGV = 9.80665
      DO 25 I = 1,NPT
      TOTN(I) = 0
      DO 25 J = 1,MS
      TOTN(I) = TOTN(I) + EN(J,I)
      25 CONTINUE
      FMT(4) = FMT(6)
      RETURN
      C
      ENTRY OUT2
      C
      C-----PRESSURE
      C
      DO 55 I=1,NPT
      K= 2*I+3
      FMT(K) = F4
      IF (PPP(I).GE.1.) FMT(K)=F3
      IF (PPP(I).GE.10.) FMT(K)=F2
      IF (PPP(I).GE.100.) FMT(K)=F1
      55 CONTINUE
      WRITE (6,FMT) (FP(I),I=1,4), (PPR(J),J=1,NPT)
      C
      C-----TEMPERATURE
      C
      DO 65 I=1,NPT
      NV(I) = TTI(I)*.5
      65 CONTINUE
      FMT(4) = FMT13
      FMT(5) = FMT19
      WRITE (6,FMT) (FI(I),I=1,4), (NV(J),J=1,NPT)
      C
      C-----ENTHALPY
      C
      DO 75 I=1,NPT

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P1712 01582  
 P1712 01583  
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 P1712 01633  
 P1712 01634

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      V(I) = HSUM(I) * R
      75 CONTINUE
      FMT(5) = F9
      FMT(7) = F1
      WRITE (6,FMT) (FM(I), I=1,4), (V(J), J=1,NPT)
      C
      C ENTROPY
      C
      C
      FMT(7) = F4
      DO 78 I = 1,NPT
      V(I) = SSUM(I) * R
      78 CONTINUE
      WRITE (6,FMT) (FS(I), I=1,4), (V(J), J=1,NPT)
      WRITE (6,80)
      80 FORMAT ( 1H )
      C
      C MOLECULAR WEIGHT
      C
      FMT(7) = F3
      WRITE (6,FMT) (FM(I), I=1,4), (WM(J), J=1,NPT)
      C
      C (DLV/DLP) T
      C
      FMT(7) = F5
      IF (EQL) WRITE (6,FMT) (FV(I), I=1,4), (DLVPT(J), J=1,NPT)
      C
      C (DLV/DLT) P
      C
      FMT(7) = F4
      IF (EQL) WRITE (6,FMT) (FO(I), I=1,4), (DLVTP(J), J=1,NPT)
      C
      C HEAT CAPACITY
      C
      DO 85 I = 1,NPT
      V(I) = CPR(I) * R
      85 CONTINUE
      WRITE (6,FMT) (FG(I), I=1,4), (VT(J), J=1,NPT)
      C
      C GAMMA(S)
      C
      WRITE (6,FMT) (FG(I), I=1,4), (GAMMAS(J), J=1,NPT)
      C
      C SONIC VELOCITY
      C
      FMT(7) = F1
      DO 95 I = 1,NPT
      SONVEL(I) = SORT(R3 * GAMMAS(I) * TTT(I) / WM(I))
      95 CONTINUE
      WRITE (6,FMT) (FL(I), I=1,4), (SONVEL(J), J=1,NPT)
      VOLUME = GAMMAS(1) * TTT(1)
      IMPETUS = VOLUME * 2781. / WM(1)
      RETURN
      C

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P1712 01635  
 P1712 01636  
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 P1712 01686  
 P1712 01687

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160  ENTRY OUT1
    IF (.NOT.EOL) GO TO 331
    C
    C MOLE FRACTIONS - EQUILIBRIUM
    C
165  WRITE (6,80)
    PRINT*,F5
    WRITE(6,310)
    310 FORMAT(15HMOLE FRACTIONS //)
    DO 330 K=1,NS
    DO 315 I=1,NPT
    V(I) = EN(K,I) /TOTN(I)
    315 CONTINUE
    DO 316 I=1,NPT
    IF (V(I).GE.(5.E-6)) GO TO 320
    316 CONTINUE
    320 WRITE (6,FMT) SUB(K,1),SUB(K,2),SUB(K,3),FB,(V(I),I=1,NPT)
    330 CONTINUE
    331 WRITE(6,335)
    335 FORMAT(11SHADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MO
    1LE FRACTIONS WERE LESS THAN .00005 FOR ALL ASSIGNED CONDITIONS//)
    LINE= 0
    DO 350 K=1,NS
    DO 340 I=1,NPT
    IF ((EN(K,I)/TOTN(I)).GE.(5.E-6)) GO TO 343
    340 CONTINUE
    LINE= LINE+1
    Z(LINE,1) = SUB(K,1)
    Z(LINE,2) = SUB(K,2)
    Z(LINE,3) = SUB(K,3)
    343 IF ((LINE.NE.10) .AND. K.NE.NS) GO TO 350
    IF (LINE.EQ.6) GO TO 1800
    WRITE(6,345) (Z(LN,1),Z(LN,2),Z(LN,3),LN=1,LINE)
    345 FORMAT (10(1X,3A4))
    LINE= 0
    350 CONTINUE
    IF (.NOT.MOLES) WRITE(6,360)
    360 FORMAT(78HNOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXI
    2DANT IN TOTAL OXIANTS )
    WRITE(6,1100) MOLE
    1100 FORMAT(1H0.*VISCOSITY AND CONDUCTIVITY VALUES BASED ON *.F5.1.* PE
    ARGENT-OF GAS MIXTURE*)
    1000 RETURN
    END

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SUBROUTINE	RATIO	FORTRAN EXTENDED VERSION 2.0	31/12/70	08.09.56.	PAGE NO. 1
		SUBROUTINE RATIO			
	C	USED FOR AREA RATIO INTERPOLATION ONLY		P1712 01730	
	C			P1712 01731	
	C			P1712 01732	
	C			P1712 01733	
05	C	DOUBLE PRECISION G.X		P1712 01734	
	C	LOGICAL EQL, FROZ, TPSP		P1712 01735	
	C			P1712 01736	
10	C	DIMENSION PER(2,2), AI(13), APCP(13), AT(13), ANMT(13), RP(2), NV(13)		P1712 01737	
	C	1, RPP(2)		P1712 01738	
	C	COMMON/POINTS/NSUM(13), SSUM(13), CPR(13), OLVP(13), OLVP(13)		P1712 01739	
	C	1, GAMMAS(13), P(26), T(26), V(13), PPP(13), MM(13), SONVEL(13), TTT(13)		P1712 01740	
	C	2, FCTN(13)		P1712 01741	
15	C	COMMON/SPECES/COEF(2,7,150), S(150), EN(150,13), ENLN(150), HQ(150)		P1712 01742	
	C	1, DELN(150), A(15,150), SUB(150,3), IUSE(150), TEMP(150,2)		P1712 01743	
	C	COMMON/MISC/ENN, SUMN, TT, S9, ATOM(3,101), LLMT(15), BU(15), BOP(15,2)		P1712 01744	
	C	1, TM, TLOM, THIO, THIGH, PP, CPSUM, OF, EQNAT, FPCT, R, RR, HSUBU, AC(2), AM(2)		P1712 01745	
	C	2, HPP(12), RHU(2), VMIN(2), VPLS(2), MP(2), DATA(22), NAME(15,5)		P1712 01746	
	C	3, ANMT(13), PCNT(13), ENTMT(13), FAZ(13), RTEMT(13), FOX(15), DENST(13)		P1712 01747	
20	C	4, RHOP, KMM(15), TLN, JANF		P1712 01748	
	C	COMMON/DOUBLE/ G(20,21), X(20)		P1712 01749	
	C	COMMON/INDX/ IOLEBUG, CONVG, IP, HP, SP, MPSP, TPSP, MOLES, NP, NT, NPT, L, NS,		P1712 01750	
	C	1, IMAT, IMAT, IOIN, J, NONIT, IP, NEWR, NSUB, NSUP, ITN, CPCVFR, CPCVELJ		P1712 01751	
	C	2, IONS, NC, NSERT, JSOL, JULIQ, KASE(14), JREAC, IC, IQ2		P1712 01752	
25	C	COMMON/PCP/PCP(26), VMOCT(13), SPMT(13), YAGI(13), SUBAK(13), SUPAK(13)		P1712 01753	
	C	1, CPRF(13), AEAT(13), CSTR, EQL, FROZ, SS0		P1712 01754	
	C	COMMON/OUT/OUT(13), F(4), FT(4), FM(4), FS(4), FH(4), FV(4), FO(4)		P1712 01755	
	C	1, FC(4), FG(4), FB, FMT(13), F1, F2, F3, F4, F5, FL(4), FMT9, FAL, FA2		P1712 01756	
	C	2, FRA, FC1, FN(4), F1(4), FA(4), FI(4), F19X, F0		P1712 01757	
30	C			P1712 01758	
	C			P1712 01759	
	C	EQUIVALENCE(I, NV)		P1712 01760	
	C			P1712 01761	
	C	MBLO = NPT-2		P1712 01762	
35	C	DO 22 J=3, NPT		P1712 01763	
	C	IF(PCP(J), CT, PCP(2)) GO TO 30		P1712 01764	
	C	22 CONTINUE		P1712 01765	
	C	GO TO 31		P1712 01766	
30	C	NSLO=J-3		P1712 01767	
31	C	DO 1200 ISONIC=1,2		P1712 01768	
	C	LL = 1		P1712 01769	
40	C	IF(ISONIC.EQ.2) GO TO 34		P1712 01770	
	C	IF(NSUB.EQ.0) GO TO 1200		P1712 01771	
	C	NAR = NSUB		P1712 01772	
	C	GO TO 36		P1712 01773	
45	C	34 IF(NSUP.EQ.0) GO TO 1200		P1712 01774	
	C	NAR = NSUP		P1712 01775	
36	C	DO 1100 I=1, NAR		P1712 01776	
	C	IF(ISONIC.EQ.2) GO TO 40		P1712 01777	
	C	IF(NAR.O.E.1) GO TO 1100		P1712 01778	
50	C	K=2+MBLO		P1712 01779	
	C	DO 36 JJ=4, K		P1712 01780	
	C	J=JJ		P1712 01781	
	C	V(LL) = SUBAR(I)		P1712 01782	

SUBROUTINE	RATIO	FORTAN EXTENDED VERSION 2.0	31/12/70	08.09.56.	PAGE NO. 2
55	IFV(LL),GE,AEAT(J); GO TO 56			P1712 01783	
	38 CONTINUE			P1712 01784	
	GO TO 56			P1712 01785	
40	IF(NPT-NBL0,LE,3) GO TO 1100			P1712 01786	
	V(LL) = SUPAR(1)			P1712 01787	
	K=4*NSLO			P1712 01788	
60	DO 42 JJ=K,NPT			P1712 01789	
	J=JJ			P1712 01790	
	IF(V(LL),LE,AEAT(J)) GO TO 56			P1712 01791	
-2	CONTINUE			P1712 01792	
	IF(V(LL),GE,AEAT(J)*3.) GO TO 85			P1712 01793	
65	56 KJ = J-1			P1712 01794	
	K = KJ			P1712 01795	
	DO 64 JJ=1,2			P1712 01796	
	IF(OPR(K).NE.0.) GO TO 63			P1712 01797	
	WRITE(6,62)K			P1712 01798	
70	62 FORMAT(17H0CANNOT USE POINT,12,3X,4HCP=0 )			P1712 01799	
	GO TO 1100			P1712 01800	
61	PER(JJ,1)=-1.7CPR(K)*WM(K)			P1712 01801	
	IF (EQL) PER(JJ,1) = PER(JJ,1)*DLVTP(K)			P1712 01802	
75	PER(JJ,2) = TTT(K)/E.*WM(K)*(HSUM(1)-HSUM(K))			P1712 01803	
	RP(JJ) = 1./(1./GAMMA(K)-PER(JJ,2))			P1712 01804	
	IF(EQL)RPP(JJ) = 1.*DLVTP(K)+(1.-DLVTP(K))*PER(JJ,1)			P1712 01805	
	K = KJ + 1			P1712 01806	
64	CONTINUE			P1712 01807	
75	AMAT(LL) = WM(1)			P1712 01808	
80	CALL SET(PCP(KJ),RP(1),AEAT(KJ),V(LL), APCP(LL))			P1712 01809	
	CALL SET(TTT(KJ),PER(1,1),PCP(KJ),APCP(LL),AT(LL))			P1712 01810	
	IF(EQL)CALL SET (WM(KJ),RPP(1),PCP(KJ),APCP(LL),AMNT(LL))			P1712 01811	
	K = KJ			P1712 01812	
85	DO 74 JJ=1,2			P1712 01813	
	G(JJ,7)=SPIM(K)*2			P1712 01814	
	G(JJ+2,7)=2.*G(JJ,7)*PER(JJ,2)			P1712 01815	
	G(JJ+4,7)=(1.-GAMMA(K))/GAMMA(K)*G(JJ+2,7)			P1712 01816	
	G(JJ,1)=1.			P1712 01817	
	G(JJ+2,1)=0			P1712 01818	
90	G(JJ+4,1)=0			P1712 01819	
	G(JJ,2)=ALOG(PCP(K))			P1712 01820	
	G(JJ+2,2)=1.			P1712 01821	
	G(JJ+4,2)=0			P1712 01822	
	DO 70 P=3,5			P1712 01823	
95	MXG=M-1			P1712 01824	
	G(JJ,M)=G(JJ,2)*MXP			P1712 01825	
	MXP=MXP-1			P1712 01826	
	G(JJ+2,M)=G(JJ,2)*MXP*FLOAT(M-1)			P1712 01827	
100	G(JJ+4,M)=G(JJ+2,M)/G(JJ,2)*FLOAT(M-2)			P1712 01828	
	70 CONTINUE			P1712 01829	
	K = KJ + 1			P1712 01830	
74	CONTINUE			P1712 01831	
	INAT = 6			P1712 01832	
105	CALL MGAUSS			P1712 01833	
	AI(LL) = X (1)			P1712 01834	
	DO 84 JJ=2,6			P1712 01835	

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      AITLL=AI(1LL)*X*(J3)*ALOG(APCP(LL))*((J3-1)
      64 CONTINUE
      IF(AI(LL).LE.0.)GO TO 85
      AITLL=AITLL**0.5
      GO TO 86
      85 LL=LL-1
      86 IF(LL.GE.15)OR(I.GZ.NARY)GO TO 90
      LL=LL+1
      GO TO 1100
      C
      C OUTPLY
      C
      90 IF(EGLT)WRITE(6,87)
      87 FORMAT(1H1/20X,"* THEORETICAL GUN PROPELLANT PERFORMANCE ASSUMING E
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160      C      C*
      C
      FMT(5) = FMT19
      DO 94 M=1,LL
      NV(M)=CSIR+.5
94 CONTINUE
      WRITE(6,FMT) (FR(I),N=1,4), (NV(M),M=1,LL)
      C
      CF = THRUST COEFFICIENT
      C
      DO 95 M=1,LL
      V(PJER(I,M)*32.1747/CSIR
95 CONTINUE
      FMT(5) = F3
      FMT(7) = F3
      WRITE(6,FMT) FC1,F8,FD,FB,(V(M),M=1,LL)
      WRITE(6,96)
96 FORMAT(' ')
      C
      C      PRESSURE RATIO
      C
      FMT(4) = FMT(6)
      DO 97 M=1,LL
      K=2*M+3
      FMT(K) = F3
      IF(APCP(M).GE.1000.) FMT(K)=F2
      IF(APCP(M).GE.10000.) FMT(K)=F1
97 CONTINUE
      C
      C      PRESSURE
      C
      WRITE(6,FMT) FR1,F8,FB,FB,(APCP(M),M=1,LL)
      DO 98 M=1,LL
      K=2*M+3
      V(M)=P(1)/APCP(M)
      FMT(K) = F3
      IF(V(M).GE.1.) FMT(K)=F3
      IF(V(M).GE.10.) FMT(K)=F2
      IF(V(M).GE.100.) FMT(K)=F1
98 CONTINUE
      WRITE(6,FMT) (FF(N),N=1,4), (V(M),M=1,LL)
      C
      C      TEMPERATURE
      C
      DO 101 M=1,LL
      NV(M)=AT(M)+.5
101 CONTINUE
      FMT(5) = FMT19
      WRITE(6,FMT) (FT(N),N=1,4), (NV(M),M=1,LL)
      C
      C      ENTHALPY
      C

```

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SUBROUTINE RATIO FORTRAN EXTENDED VERSION 2.0

```

C
      FMT(5)=F8
      FMT(7)=F1
      DO 104, M=1,LL
      V(M)=MSUM(1)*R-1000.*(AI(M)/294.38)**2
104 CONTINUE
      WRITE(6,FMT) (P(M),M=1,N), (V(M),M=1,LL)
C
220  C      ENITROPY
C
      FMT(7)=F4
      V(1)=SSUM(2)*R
      DO 106, M=1,LL
      V(M)=V(1)
106 CONTINUE
      WRITE(6,FMT) (FS(M),M=1,4), (V(M),M=1,LL)
C
230  C      MOLECULAR HEIGHT
C
      FMT(7)=F3
      WRITE(6,FMT) (FM(M),M=1,4), (AMT(M),M=1,LL)
110 CONTINUE
120 CONTINUE
      RETURN
      END

```

SUBROUTINE REACT    FORTRAN EXTENDED VERSION 2.0    31/12/70    06:09.56.    PAGE NO. 1

----- SUBROUTINE REACT -----

05    C    DOUBLE PRECISION G,X  
       C    LOGICAL HP,SP,TP,IOEBUG,CONVG,NEMR,IONS,MOLES,EOL,FROZ  
       C    DIMENSION NAME(15),V(15)

10    C    COMMON/HISC/ENN,SUMN,TT,S0,ATOM(3,101),LLMT(15),80(15),80P(15,2)  
       1    TM,TLGW,THID,THIGH,PP,CPSON,OF,EQAT,FCPT,R,RR,HSUB8,AC(2),AK(2)  
       2    HPP(2),RHO(2),VWIN(2),VPLS(2),MPI(2),DATA(22),NAME(15,5)  
       3    ANUM(15,5),PECHT(15),ENTH(15),FAZ(15),RTEMP(15),FOX(15),DENS(15)  
       4    HOP,MM(15),TEN,JANE  
       C    COMMON/INDX/ IOEBUG,CONVG,IP,HP,SP,HPP,TPSP,MOLES,NP,NT,NPT,L,NS,  
       1    KMAT,IMAT,IGI,N,J,NOHIT,IP,NEMR,NSUB,NSUP,ITN,CPCVFR,CPQVEQ  
       2    IONS,NC,NSERT,JSOL,JLIQ,KASE(14),NREAC,IG,IQ2

15    C    EQUIVALENCE (NAME,ANAME)

20    C    DATA MOL/1HM/,OX/1HO/,LANK/1M /,IZERO/2H00/  
       C    WRITE(6,3000)  
       9000    FORMAT(1M,'\*REACTANTS\*')  
       DO 10 K=1,2  
       10    K=K+1  
       HPP(K)=0.  
       RHC(K)=0.  
       VPLS(K)=0.  
       VWIN(K)=0.  
       AC(K)=0.  
       AN(K)=0.  
       DO 8 J=1,15  
       LLMT(J)=0  
       BOP(J,K)=0.  
       30    C    CONTINUE  
       10    CONTINUE  
       N=1  
       L=1  
       NREACS=NREAC  
       IF (NREAC.GT.16) NREAC=16  
       DO 200 N=1,NREAC  
       20    READ(5,21) (NAME(N,I),ANUM(N,I),I=1,5),PECHT(N),MOLE,ENTH(N),FAZ(N)  
       1    RTEMP(N),FOX(N),DENS(N)  
       21    FORMAT(5(A2,F7.5),F7.5,A1,F9.5,A1,F8.5,A1,F8.5)  
       IF (L.EQ.0) GO TO 20  
       IF (NAME(N,1).EQ.LANK) GO TO 200  
       WRITE (6,31) (NAME(N,I),ANUM(N,I),I=1,5),PECHT(N),MOLE,ENTH(N),FAZ  
       1    (N),RTEMP(N),FOX(N),DENS(N)  
       31    FORMAT(1X,5(A2,1X,F7.5),F7.5,2X,11,F11.2,2X,A1,2X,F8.5,2X,  
       1A1,3X,F8.5)  
       35    IF (MOLE.EQ.MOL) MOLES=.TRUE.  
       K=2  
       IF (FOX(N).EQ.OX) K=1

40    C    P1712 01967  
       P1712 01968  
       P1712 01969  
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       P1712 02018  
       P1712 02019

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SUBROUTINE REACT FORTRAN EXTENDED VERSION 2.0

```
55      DO 38 J=1,15
          DATA(J) = 0.
          38 CONTINUE
          RM=0.
          GO 100 JJ=1,5
          IF (ANUM(N,JJ).EQ.0.) GO TO 101
          DO 41 J=1,15
              NJ = J
              IF (LLMT(J).EQ.0.) GO TO 45
              IF (NAME(N,JJ).EQ.LLMT(J)) GO TO 46
              41 CONTINUE
              45 L = NJ
              LLPT(J)=NAME(N,JJ)
              46 DO 48 KK=1,101
                  IF (ATOM(1,KK).EQ.ANAME(N,JJ)) GO TO 50
                  48 CONTINUE
                  L=0
                  GO TO 20
              50 RM=RM+AMU(N,JJ)*ATOM(2,KK)
                  V(J)=ATOM(3,KK)
                  DATA(J)=ANUM(N,JJ)
              100 CONTINUE
              101 PCMT=PECHT(N)
                  IF (MOLES) PCMT=PCMT*RM
                  MP(NT=MP(T)+PCMT
                  IF (NAME(N,5).NE.1ZER0) HPP(K)=HPP(K)+ENTH(N)*PCMT/RM
                  AM(K)=AM(K)+PCMT/R4
                  DO 110 J=1,L
                      80 F(J,K)=DATA(J)*PCMT/RM +90P(J,K)
                      80 CONTINUE
                  110 CONTINUE
                  IF (DENSE*NE.0.) GO TO 115
                      GO TO 117
                  115 RHO(K)=RHO(K)+PCMT/DENS(N)
                  117 RMK(N) = RM
                  200 CONTINUE
                  IF (NREAGS.LE.16) GO TO 1205
                      NREA=NREAGS-16
                      DO 1200 I=1,NRAC
                          1200 READ(5,21) JUNK
                          1205 IF (L.EQ.0) GO TO 1000
                              IF (L.EQ.0) GO TO 1000
                              DO 220 K=1,2
                                  IF (MP(K).EQ.0.) GO TO 220
                                  HPP(K)=HPP(K)/NF(K)
                                  AM(K) = MP(K)/AM(K)
                                  IF (RHO(K).NE.0.) RHO(K)=MP(K)/RHO(K)
                                  DO 215 J=1,L
                                      80 P(J,K)=80P(J,K)/MP(K)
                                  IF (V(J).GT.0.) VPM(K)=VPM(K)+80P(J,K)*V(J)
                                  IF (V(L).GT.0.) VPLS(K)=VPLS(K)+80P(J,K)*V(J)
                                  215 CONTINUE
                                  IF (MOLES) GO TO 220
                                  DO 216 N=1,NREAL
```

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SUBROUTINE REACT FORTRAN EXTENDED VERSION 2.0

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110 IF (FOX(N) = 0.0X.AND.N.EQ.2) GO TO 218
    IF (FOX(N) .NE. 0X.AND. L.EQ.1) GO TO 218
    PECMT(N) = PECMT(N)/WP(K)
    218 CONTINUE
    220 CONTINUE
    NEWR = TRUE.
    DO 230 N = 1, NREAC
        IF (DENS(N) .NE. C.) GO TO 230
        RHC (1) = 0.
        GO TO 1800
    230 CONTINUE
    1000 RETURN
    END

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 P1712 02085



SUBROUTINE RKTOU		SUBROUTINE RKTOU	
C	ROCKET PERFORMANCE PARAMETERS	P1712	02086
C		P1712	02087
C		P1712	02088
C		P1712	02089
05		P1712	02090
C	LOGICAL EUL,FROZ ,TP,HP,SP,HPSP,TPSP,SHOCK	P1712	02091
C		P1712	02092
	DIMENSION NV(13),Z(10,4)	P1712	02093
	DIMENSION VELOC(13)	P1712	02094
10		P1712	02095
C	COMMON/POINTS/HSUM(13),SSUM(13),CPR(13),DLVTP(13),DLVPT(13)	P1712	02096
	1 ,GAMMA(13),P(26),I(26),V(13),PP(13),MM(13),SONVEL(13),FII(13)	P1712	02097
	2 ,ICTW(13)	P1712	02098
15		P1712	02099
	COMMON/SPECES/COEF(2,7,150),S(150),EN(150,13),FMLN(150),MO(150)	P1712	02100
	1 ,DELN(150),A(15,150),SUB(150,3),IUSE(150),TEMP(50,2)	P1712	02101
	COMMON/MLSC/EN,SUMN,IT,S0,ATOM(3,101),ALLMT(15),BO(15),60P(15,2)	P1712	02102
	1 ,TM,TLOM,TMID,THIGH,PP,CPSUM,OF,EOKAT,FPCT,R,TR,HSUBD,AC(2),AM(2)	P1712	02103
	2 ,HPP(2),RHO(2),VMIN(2),VPLS(2),HP(2),DATA(22),NAME(15,5)	P1712	02104
	3 ,TRUNT(15,5),PECHT(15),ENTHT(15),FAZ(15),RTERP(15),FOX(15),DENS(15)	P1712	02105
20		P1712	02106
	4 ,RHOP,RMW(15),TLN,JANF	P1712	02107
	COMMON/INOX/ IOEBUG,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,NP,NT,NPT,L,NS,	P1712	02108
	1 ,KAT,IMAT,IQ1,N,J,NOMIT,IP,NEWR,NSUB,NSUP,ITA,CPCVFR,CPCVEQ	P1712	02109
	2 ,IONS,NC,NSERT,JSOL,JLIO,KASE(14),NREAC,IC,I02	P1712	02110
	COMMON/PERF/PCP(26),VMOC(13),SPIM(13),VACI(13),SUBAR(13),SUPAR(13)	P1712	02111
25		P1712	02112
	1 ,CPRF(13),DEAT(13),CSTR,EUL,FROZ,SSO	P1712	02113
	COMMON/DOUP/FPMT(30),FP(4),FI(4),FH(4),FS(4),FM(4),FV(4),FO(4)	P1712	02114
	1 ,FC(4),FG(4),FB,FM13,FI,F2,F3,F4,F5,FL(4),FNTI9,FAL,FA2	P1712	02115
82		P1712	02116
	2 ,FRI,FC1,FN(4),FR(4),FA(4),FI(4),FMI9X,F3	P1712	02117
30	COMMON/CVOLUM/ VOLUMC,IMPETUS,IFLGGG	P1712	02118
	REAL IMPETUS	P1712	02119
	EQUIVALENCE (V,NV),(Z,MO)	P1712	02120
35		P1712	02121
	DATA EXIT/4HEXIT/	P1712	02122
40		P1712	02123
	IF(EQL) WRITE (6,37)	P1712	02124
	37 FORMAT(1H120X,*,THEORETICAL GUN PROPELLANT PERFORMANCE ASSUMING F	P1712	02125
	1 EQUILIBRIUM COMPOSITION DURING EXPANSION	P1712	02126
	IF (.NOT.EQL) WRITE (6,38)	P1712	02127
	38 FORMAT(1H120X,*,THEORETICAL GUN PROPELLANT PERFORMANCE ASSUMING F	P1712	02128
	1 FROZEN COMPOSITION DURING EXPANSION	P1712	02129
	IF (TPSP) WRITE (6,737)	P1712	02130
	737 FORMAT (12X,20MAT AN ASSIGNED TEMPERATURE	P1712	02131
45		P1712	02132
	V(1) = PPP(1)*14.696006	P1712	02133
	WRITE (6,40) V(1)	P1712	02134
	40 FORMAT(5H PC = ,F8.1,5H PSIA)	P1712	02135
	CALL OUT1	P1712	02136
	NEX = NPT - 2	P1712	02137
50		P1712	02138
	DO 862 I = 1,NEX	P1712	02139
	862 V(1) = EXIT	P1712	02140
	WRITE(6,48) (V(I),I=1,NEX)	P1712	02141
	48 FORMAT(1H0,16X,16HCHAMBER THROAT ,11(5X,A4))	P1712	02142
		P1712	02143



110	C	FMT(4) = FMT9X FMT(5) = FMT13 FMT(6) = FMT19 FMT(7) = F8 WRITE(6,FMT)(FR(I),I=1,4),(NV(J),J=2,NPT)	P1712 02191 P1712 02192 P1712 02193 P1712 02194 P1712 02195 P1712 02196 P1712 02197
115	C	CF = THPST COEFFICIENT FMT(6) = FMT(8) FMT(7) = F3 DO 212 I=2,NPT	P1712 02196 P1712 02196 P1712 02199 P1712 02200 P1712 02201 P1712 02202
120	C	212 V(I)=32.174*SPIK(I)/CSTR WRITE(6,FMT)FC1,FB,FB,FB,(V(J),J=2,NPT)	P1712 02203 P1712 02204 P1712 02205 P1712 02206 P1712 02207 P1712 02208
125	C	AREA RATIO FMT(5) = F8 DO 214 I = 2,NPT K = 2*1+3 FMT(K) = F4 IF (AEAT(I).GE.1.) FMT(K) = F3 IF (AEAT(I).GE.10.) FMT(K) = F2 IF (AEAT(I).GE.100.) FMT(K) = F1	P1712 02209 P1712 02210 P1712 02211 P1712 02212 P1712 02213 P1712 02214 P1712 02215
130	C	214 CONTINUE WRITE(6,FMT)FA1,FA2,FB,FB,(AEAT(J),J=2,NPT)	P1712 02216 P1712 02217 P1712 02218 P1712 02219 P1712 02220
135	C	VACUUM IMPULSE FMT(5) = FMT13 FMT(7) = F1 WRITE(6,FMT)(FA(I),I=1,4),(VAGI(J),J=2,NPT)	P1712 02221 P1712 02222 P1712 02223 P1712 02224 P1712 02225 P1712 02226
140	C	SPECIFIC IMPULSE WRITE(6,FMT)(F1(I),I=1,4),(SPIM(J),J=2,NPT)	P1712 02227 P1712 02228 P1712 02229 P1712 02230 P1712 02231 P1712 02232
145	C	WRITE(6,208) FMT(4) = F8 FMT(5) = FMT13 FMT(7) = F5 IF(COL) GO TO 312 WRITE(6,310)	P1712 02233 P1712 02234 P1712 02235 P1712 02236 P1712 02237 P1712 02238
150	C	310 FORMAT(15H0MOLE FRACTIONS //)	P1712 02239 P1712 02240 P1712 02241 P1712 02242 P1712 02243
155	C	MOLE FRACTIONS - FROZEN LINE = 0 DO 431 K=1,MS V(LINE+1) = EN(K,1)/TOTN(1) IF (V(LINE+1).LT.(9.E-6)) GO TO 424 LINE = LINE+1 24LINE,1) = SUB(K,1)	P1712 02240 P1712 02241 P1712 02242 P1712 02243

SUBROUTINE RKTOUT    FORTRAN EXTENDED VERSION 2.0		31/12/70	08.09.96.	PAGE NO. 4
160	Z(LINE,2) = 3(K,2) Z(LINE,3) = SUB(K,3) Z(LINE,4) = V(LINE)		P1712 02244 P1712 02245 P1712 02246	
424	IF (LINE.NE.4.AND.K.NE.NS) GO TO 430 IF (LINE.EQ.0) GO TO 312 WRITE (6,426) (Z(LN,1),Z(LN,2),Z(LN,3),Z(LN,4),LN=1,LINE)		P1712 02247 P1712 02248 P1712 02249	
165	426 FORMAT (1X,4I5A,7F9.5,7X) LINE = 0		P1712 02250 P1712 02251	
	430 CONTINUE		P1712 02252	
	712 CALL OUT3		P1712 02253	
170	1000 RETURN END		P1712 02254 P1712 02255	



SUBROUTINE ROCKET FORTRAN EXTENDED VERSION 2.0		31/12/70	08:09.56:	PAGE NO. 2
55	GO TO 311 309 NP = 2 DO 310 I=1,24 IF (I.GT.2) GO TO 309 IF ((PCP(I).EQ.0.)OR.PCP(I).EQ.1.) GO TO 310 309 IF (PCP(I).EQ.0.) GO TO 311 NP = NP + 1 P(NP) = P(1)/PCP(I) 310 CONTINUE 311 NSUB=0 NSUP = 0 DO 320 I=1,13 IF (SUBART(I).NE.0.) NSUB=NSUB+1 IF (SUPART(I).NE.0.) NSUP=NSUP+1 320 CONTINUE WRITE (6,RTINP) SS0 = 0. ITROT = 3 IT = 1 C C C SET ASSIGNED P DO 902 IP = 1, NP PP = P(IP) CALL EQLORN T(NPT) = IT IF (IT.NE.0.) GO TO 333 IF (NPT.EQ.0) GO TO 1000 GO TO 900 333 PCP(NPT) = P(1)/PP IF (IP.GT.1) GO TO 199 C C C COMBUSTION CHAMBER TP = .FALSE. MP = .FALSE. SP = .TRUE. S0 = SSUM(1) PCP(2) = ((GAMMAS(1)+1.) / 2.) * ((GAMMAS(1) / (GAMMAS(1)-1.)) P(2) = P(1) / PCP(2) IT = 2 * IT / (GAMMAS(1)+1.) GO TO 900 199 IF (IP.GT.2) GO TO 900 C C C THROAT 190 IF (ITH.NE.2) GO TO 191 ITH = 2 GAMMAS(2) = 0. GO TO 900 191 OH = HSUM(1)-HSUM(2) DHSTAR = OH-GAMMAS(2) * IT * ENN / 2. IF (IDEPUG) WRITE (6,923) DHSTAR, HSUM(1), HSUM(2), PCP(2)	P1712 02309 P1712 02310 P1712 02311 P1712 02312 P1712 02313 P1712 02314 P1712 02315 P1712 02316 P1712 02317 P1712 02318 P1712 02319 P1712 02320 P1712 02321 P1712 02322 P1712 02323 P1712 02324 P1712 02325 P1712 02326 P1712 02327 P1712 02328 P1712 02329 P1712 02330 P1712 02331 P1712 02332 P1712 02333 P1712 02334 P1712 02335 P1712 02336 P1712 02337 P1712 02338 P1712 02339 P1712 02340 P1712 02341 P1712 02342 P1712 02343 P1712 02344 P1712 02345 P1712 02346 P1712 02347 P1712 02348 P1712 02349 P1712 02350 P1712 02351 P1712 02352 P1712 02353 P1712 02354 P1712 02355 P1712 02356 P1712 02357 P1712 02358 P1712 02359 P1712 02360 P1712 02361		



SUBROUTINE ROCKET    FORTRAN EXTENDED VERSION 2.0    31/12/70    08.09.56.    PAGE NO. 4  
160    ~~END~~    ~~P1712~~    ~~02419~~





```
55      00 168 I=1,L
      IF(LLMT(I).EQ.MT(K)) GO TO 820
      168 CONTINUE
      00 819 J=1,L
      819 A(J,NS) = 0.
      GO TO 7
      80 020 ATT(NS)= 819
      025 IF(NS.EQ.HAXNS) GO TO 870
      IUSE(NS)= 0
      IF(PHAZ.EQ.GAS) GO TO 170
      NC= NC+1
      TEMP(NC,1)= T1
      TEMP(NC,2)= T2
      IX= IX+1
      IF(IUSE(NS-1).EQ.0 .OR. NC.EQ.1) GO TO 145
      00 830 I=1,L
      IF(A(I,NS).NE.A(I,NS-1)) GO TO 145
      830 CONTINUE
      IX= IX+1
      145 IUSE(NS)= -IX
      170 NS= NS+1
      GO TO 7
      75 970 WRITE(6,871) (SUB(NS,J),J=1,3)
      871 FORMAT(45H0DIMENSIONS IN/SPECIES/100 SHALL TO CONSIDER ,3A4)
      GO TO 7
      171 NS= NS-1
      MEMR= .FALSE.
      WRITE(6,172)
      172 FORMAT(42H0SPECIES BEING CONSIDERED IN THIS SYSTEM )
      00 174 I=1,NS,5
      15= 1+4
      85 IF(NS.LT.15) I5=NS
      174 WRITE (6,176) (DATE(1,J),DATE(2,J),SUB(J,1),SUB(J,2),SUB(J,3),J=1,
      1 I5)
      176 FORMAT(5(5X,2A3,2X,3A4))
      RETURN
      90  END
```

08.09.56.

31/12/70

FORTHAN EXTENDED VERSION 2.0

SUBROUTINE SET

```

SUBROUTINE SET(ONE,TWO,THREE,ARG,MAL)
C
C      USED FOR AREA RATIO INTERPOLATION ONLY
C      SETS UP ALL 4 BY 5 MATRICES
05  C      DOUBLE PRECISION A,ANS,G,X
C
C      DIMENSION ANS(6),ONE(2),TWO(2),THREE(2),A(20,21)
C
C      COMMON/DOUBLE/G(20,21),X(20)
C      COMMON/INDEX/ IDEBUS,CONVG,TP,HP,SP,HPSP,TPSP,MOLES,MP,NT,NPT,I,ANS,
1      KMAT,IMAT,IC1,N,J,NOMIT,IF,NEWR,NSUB,NSUP,ITN,CPCVFR,CPCVEQ
2      IONS,TMO,INSEF,JSOI,JIU,KASE(14),NREAC,IC,IO2
C
C      EQUIVALENCE (G,A),(X,ANS)
C
C      DO 8 J=1,2
A(J,5)=ALOG(ONE(J))
A(J,2)=TWO(J)
A(J,3)=THREE(J)
9 CONTINUE
C      DO 1 I=1,2
A(I,1)=1.0
A(I,2)=0.0
A(I,2,2)=1.0
DO 1 J=2,3
A(I,J+1)=A(I,2)**J
NXP=J-1
A(I+2,J+1)=A(I,2)**NXP*FLOAT(J)
1 CONTINUE
IMAT=4
CALL HGAUSD
MAL=ANS(1)
SUM=ALOG(ARG)
DO 10 J=1,3
MAL=MAL+SUM**J*(ANS(J+1))
10 CONTINUE
MAL=EXP(MAL)
RETURN
END
40

```





SUBROUTINE VISCON FORTRAN EXTENDED VERSION 2.0 31/12/78 00.09.56. PAGE NO. 3

C-----CONDUCTIVITY OF MIXTURE

110 C  
 CONMIX(N)=CONMIX(N)+FMOLE(I)\*CONM(I)/SUM  
 WRITE(6,9009) VISMIX(N),CONMIX(N),N  
 9009 FORMAT(1X,2F15.11,3X,15)  
 200 CONTINUE  
 1000 CONTINUE  
 WRITE(6,2010) (VISMIX(I),I=1,NPT)  
 2010 WRITE(6,2100) (CONMIX(I),I=1,NPT)  
 2090 FORMAT(1H ,\*VISC, 5/CM-SEC\*,13F9.6)  
 2100 FORMAT(1H ,\*C, 6AL/6-SEC-K\*,13F9.6)  
 RETURN  
 END

P171201 00116  
 P171201 00117  
 P171201 00118  
 P171201 00119  
 P171201 00120  
 P171201 00121  
 P171201 00122  
 P171201 00123  
 P171201 00124  
 P171201 00125  
 P171201 00126  
 P171201 00127  
 P171201 00128

APPENDIX II  
POLYNOMIAL FIT PROGRAM

```

PROGRAM SLSCF(INPUT,OUTPUT)
  DIMENSION TT(100),CPR(100),HTR(100),STR(100)
  DIMENSION CCPR(100),CHTR(100),CSTR(100)
  DIMENSION NPT(2),NAME(6)
  COMMON/PATRIX/ G(10,11),X(10),IMAY
  R=1-99726
  ASSIGN 500 TO MEOF
  IF(EOF(MEOF)) 500,500,1
  1 READ 40,MO,NPT,NAME
  40 FORMAT(F10.1,2I3,4X,6A10)
  PRINT 112,NAME,MO
  112 FORMAT('111,29X,6A10//1P',5NH0 = ,F10.1//)
  KPT=0
  111 KPT=KPT+1
  NVAL=NPT(KPT)
  READ 6,(ITT(K),K=1,NVAL)
  READ 7,(CPR(K),K=1,NVAL)
  READ 7,(HTR(K),K=1,NVAL)
  DC 22 I=1,NVAL
  22 HTR(I)=HTR(I)+1000.*MO
  READ 7,(STR(K),K=1,NVAL)
  6 FORMAT(20F4.0)
  7 FORMAT(10F8.3)
  DC 16 I=1,10
  DC 15 J=1,11
  G(I,J)=0.
  15 CONTINUE
  16 CONTINUE
  SLT=0.
  SLT2=0.
  SLT3=0.
  SLT4=0.
  SLT5=0.
  SLT6=0.
  SLT7=0.
  SLT8=0.
  SLT9=0.
  DO 100 K=1,NVAL
    T=TT(K)
    CP=CPR(K)/R
    HT=HTR(K)/(R*T)
    ST=STR(K)/R
    TLOG=ALOG(T)
    T2=T**2
    T3=T**3
    T4=T**4
    T5=T**5
    T6=T**6
    T7=T**7
    T8=T**8
    T9=T**9
    TREC=1.0/T
    TM2=1.0/T2
    SUMT=SUMT+T
  
```



15.40.00.

05/01/71

FURTRAN EXTENDED VERSION 2.0

PROGRAM

SLSQF

```

SUMT2=SUMT2+T2
SUMT3=SUMT3+T3
SUMT4=SUMT4+T4
SUMT5=SUMT5+T5
SUMT6=SUMT6+T6
SUMT7=SUMT7+T7
SUMT8=SUMT8+T8
SUMT2=SUMT2+TM2
G(1,1)=G(1,1)+2.*TLOG**2
G(1,2)=G(1,2)+(1.5+TLOG)*T
G(1,3)=G(1,3)+(4./3.+5.*TLOG)*T2
G(1,4)=G(1,4)+(1.25+TLOG/3.)*T3
G(1,5)=G(1,5)+(1.2+TLOG/4.)*T4
G(1,6)=G(1,6)+TREC
G(1,7)=G(1,7)+TLOG
G(1,11)=G(1,11)+(CP+HT+ST+TLOG
G(2,11)=G(2,11)+(CP+5*HT+ST)*T
G(3,11)=G(3,11)+(CP+HT/3.+5*ST)*T2
G(4,11)=G(4,11)+(CP+HT/4.+ST/3.)*T3
G(5,11)=G(5,11)+(CP+HT/5.+ST/4.)*T4
G(6,11)=G(6,11)+HT*TREC
G(7,11)=G(7,11)+ST
IF(X.GT.1) GO TO 50
G(1,8)=1.0
G(1,9)=1.0
G(1,10)=TLOG
G(2,6)=FLOAT(INVAL)/2.0
G(2,8)=T
G(2,9)=1/2.0
G(2,10)=1
G(3,8)=12
G(3,9)=12/3.
G(3,10)=1/2.
G(4,8)=13
G(4,9)=13/4.
G(4,10)=13/3.
G(5,8)=14
G(5,9)=14/5.
G(5,10)=1/4.
G(6,9)=TREC
G(7,7)=FLOAT(INVAL)
G(7,10)=1.0
G(8,11)=CP
G(9,11)=HT
G(10,11)=ST
50 CONTINUE
100 CONTINUE
G(2,2)=G(2,2)+4.*SUMT2
G(2,3)=(5./3.)*SUMT3
G(2,4)=(35./24.)*SUMT4
G(2,5)=(27./20.)*SUMT5
G(2,7)=SUMT
G(3,3)=(49./36.)*SUMT4
```



PROGRAM	SLSQF	FURTRAN EXTENDED VERSION 2.0	05/01/71	15.40.08.	PAGE NO. 4
160	411	FORMAT(1H,1X,F5.0,9F8.3) PRINT 411,IT(1),CPR(1),CCPR(1),DIR,CHTR(1),STR(1),CSIR(1),DCPR, 1CHTR,OSTR			
165	410	CCTINUE GC 10 (111,1),KPT 500 CONTINUE END			

SUBROUTINE MGAUSD

C SOLVE ANY LINEAR SET OF UP TO 20 EQUATIONS

C DOUBLE PRECISION G,X,COEFX(20),SUM,Z  
C DIMENSION COEFX(20)

C COMMON/MATRIX/ G(10,10),X(10),IMAT

C EQUIVALENCE (IUSE,IMAT)

C DATA SIGNO/1.E+38/  
C DATA SIGNO/1.E+320/

C BEGIN ELIMINATION OF NTH VARIABLE

C IUSE1=IUSE+1

C DO 45 NN=1,IUSE  
C IF (NN-IUSE) 8,83,8  
C 83 IF (G(NN,NN)) 31,23,31

C SEARCH FOR MAXIMUM COEFFICIENT IN EACH ROW

C DO 10 I=NN,IUSE

C COEFX(I) = BIGNO  
C IF (G(I,NN).EQ.0.) GO TO 10  
C COEFX(I) = 0.  
C DO 10 J=NN,IUSE1  
C SUM = G(I,J)

C IF (SUM-11.7-1) SUM=-SUM  
C IF (J.NE.NN) GO TO 9  
C Z = SUM

C GO TO 10  
C 9 IF (SUM.GT.COEFX(I)) COEFX(I)=SUM

C 10 CONTINUE

C COEFX(I) = COEFX(I)/Z

C 10 CONTINUE

C TEMP = BIGNC

C I=0

C 20 DO 22 J=NN,IUSE

C IF (COEFX(J)-TEMP) 87,22,22

C 87 TEMP=COEFX(J)

C 1=J

C 22 CONTINUE

C IF (I) 20,23,28

C INDEX I LOCATES EQUATION TO BE USED FOR ELIMINATING THE NTH  
C VARIABLE FROM THE REMAINING EQUATIONS

C INTERCHANGE EQUATIONS I AND NN

C 28 IF (NN-I) 29,31,29

C 29 DO 30 J=NN,IUSE1

```

55      Z=G(I,J)
      G(I,J)=G(MN,J)
      G(MN,J)=Z
      30 CONTINUE
C
60      C-----DIVIDE MTH ROW BY MTH DIAGONAL ELEMENT AND ELIMINATE THE MTH
      C      VARIABLE FROM THE REMAINING EQUATIONS
      C
      31 K = MN + 1
      DO 36 J = K, IUSE1
      IF((I(MN,MN).EQ.0.) GO TO 23
      G(MN,J) = G(MN,J) / G(MN,MN)
      36 CONTINUE
      IF(K-IUSE1) 88,45,88
      88 DO 44 I = K,IUSE
      40 DO 44 J = K, IUSE1
      G(I,J) = G(I,J) - G(I,MN)*G(MN,J)
      44 CONTINUE
      45 CONTINUE
C
75      C      BACKSOLVE FOR THE VARIABLES
      C
      47 J = K - 1
      K = IUSE
      X(K) = 0.000
      X(K) = 0.0
      SUM = 0.0
      IF(IUSE - J) 51,48,48
      48 DO 50 I = J,IUSE
      SUM = SUM + G(K,I)*X(I)
      50 CONTINUE
      51 X(K) = G(K,IUSE1) - SUM
      K = K - 1
      IF (K) 47,151,47
      23 IUSE = IUSE-1
      151 RETURN
      END
90

```

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